

# Aerosol Technology Basics

What's Particle?

# Introduction

- The word aerosol was coined about 1920 as an analog to the term hydrosol, a stable liquid suspension of solid particles. Aerosols are also referred to as suspended particulate matter, aerocolloidal system, and disperse systems.

**TABLE 1.1 Types of Particulate Suspensions**

Suspending Medium	Type of Suspended Particles		
	Gas	Liquid	Solid
Gas	—	Fog, mist, spray	Fume, dust
Liquid	Foam	Emulsion	Colloid, suspension, slurry
Solid	Sponge	Gel	Alloy

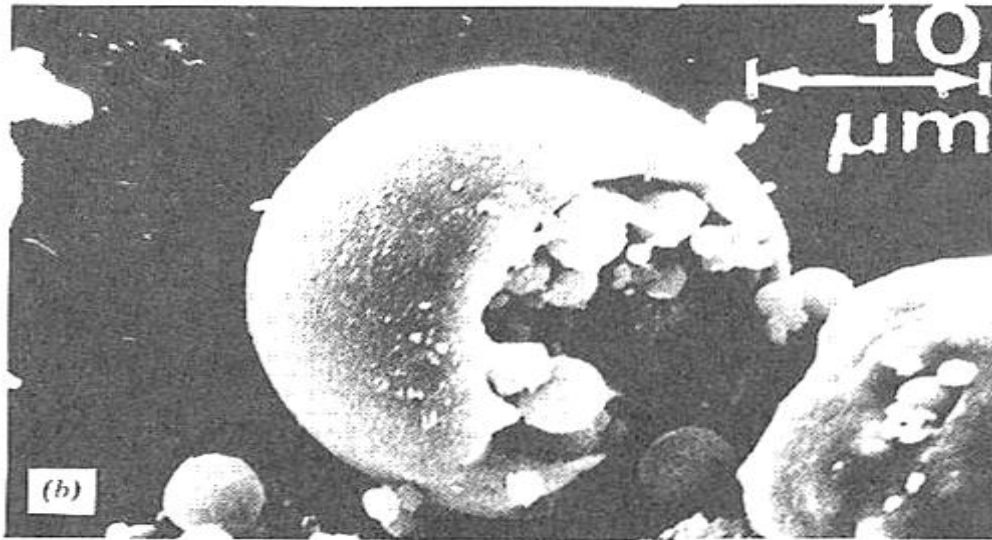
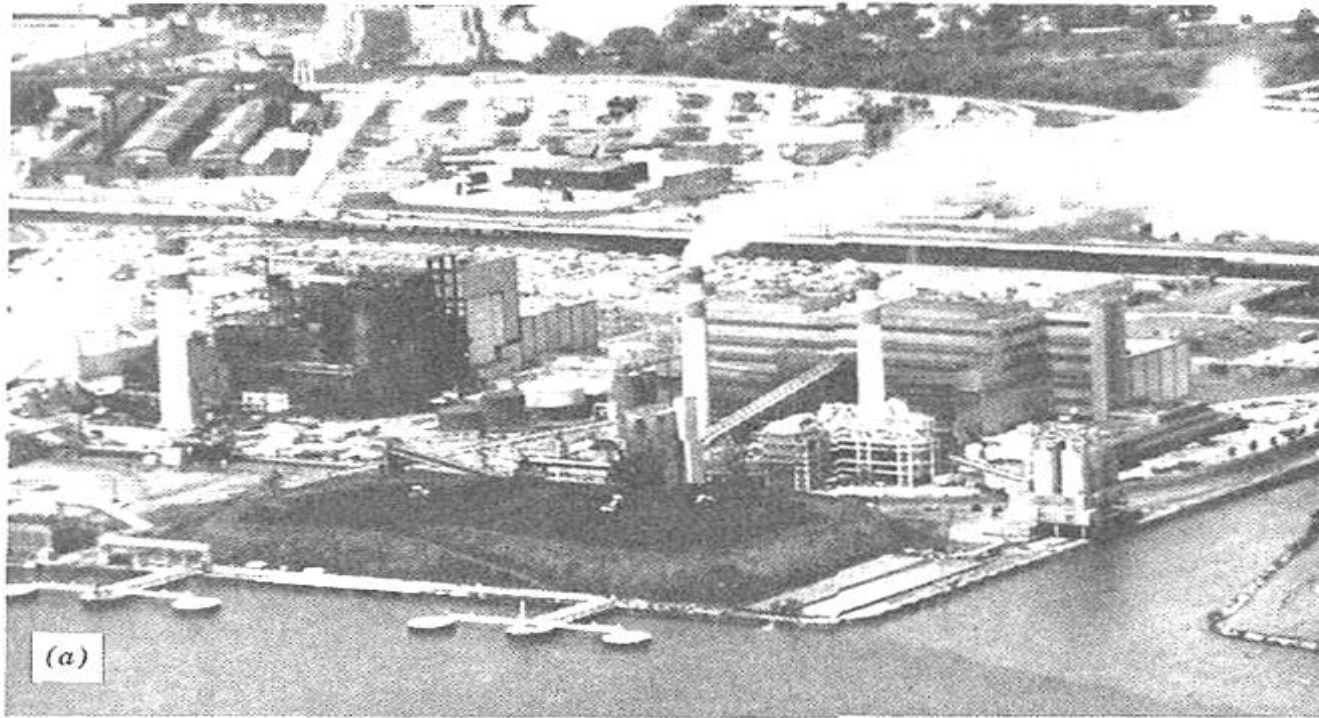
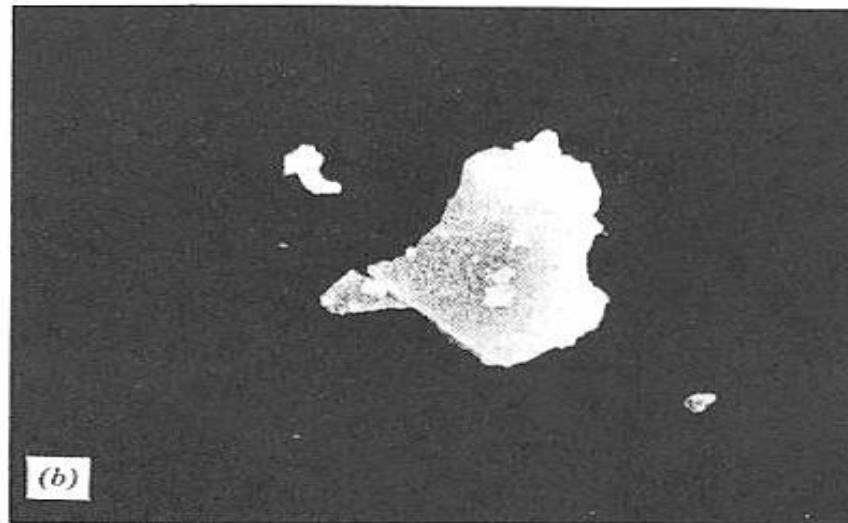
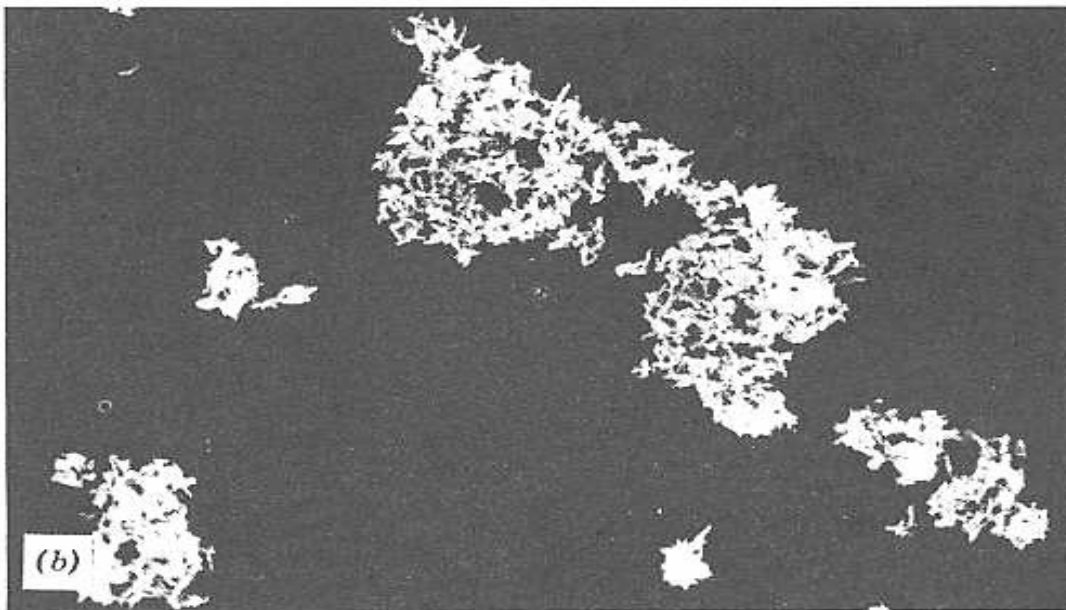
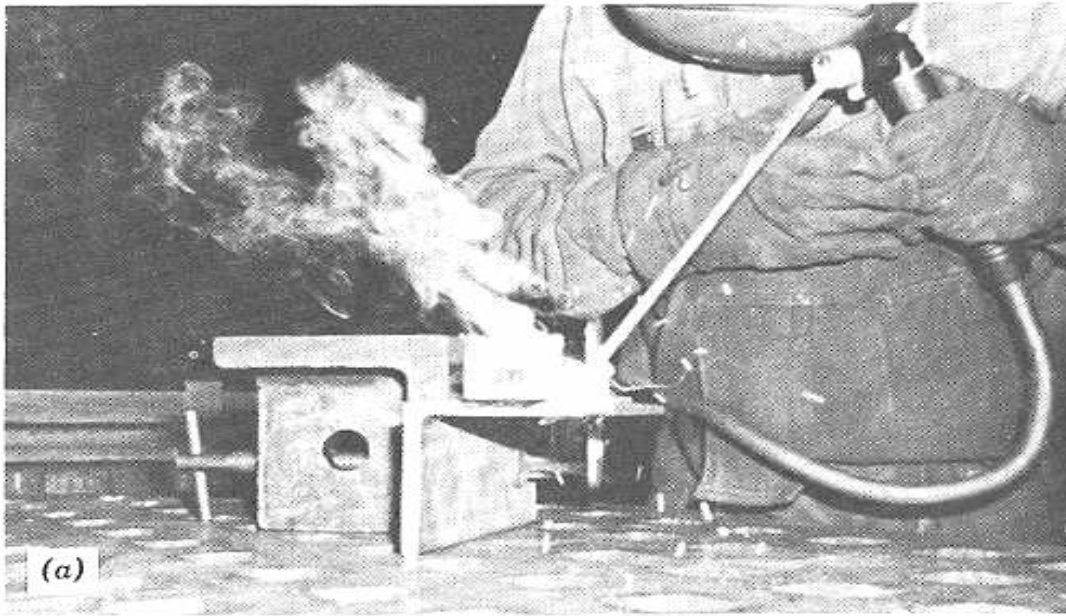


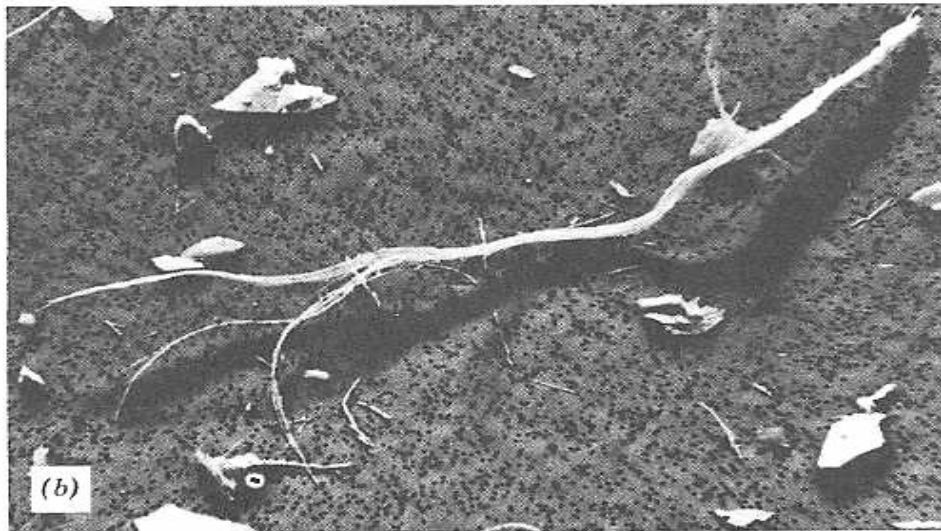
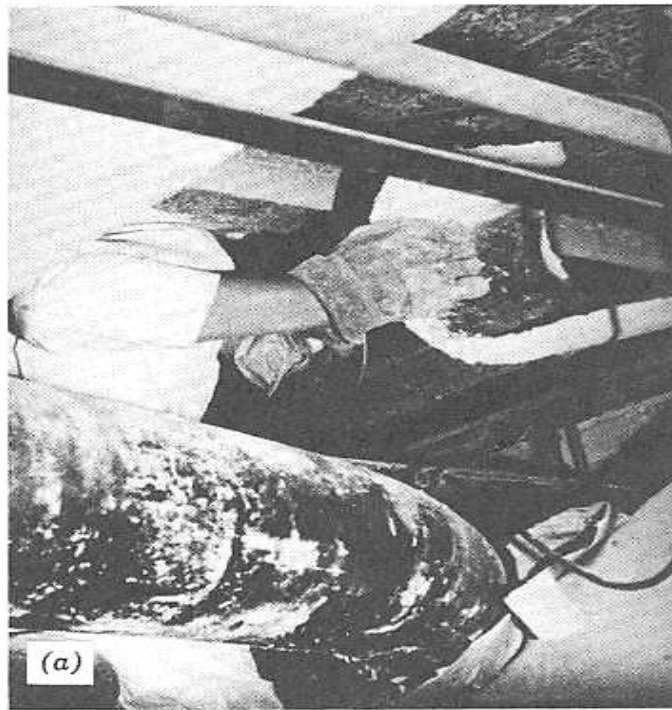
FIGURE 1.1 (a) Coal-burning power plant. (b) Scanning electron microscope (SEM) photograph of coal fly ash particles.



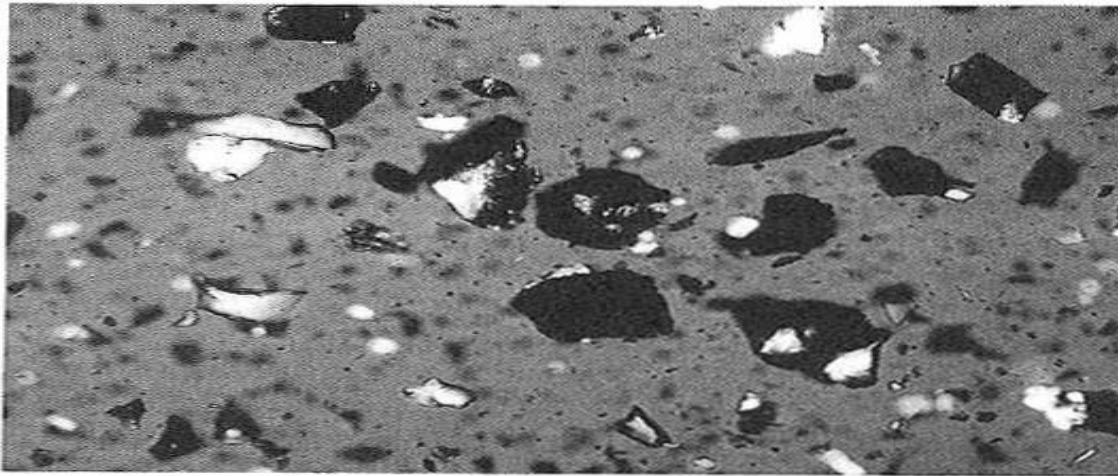
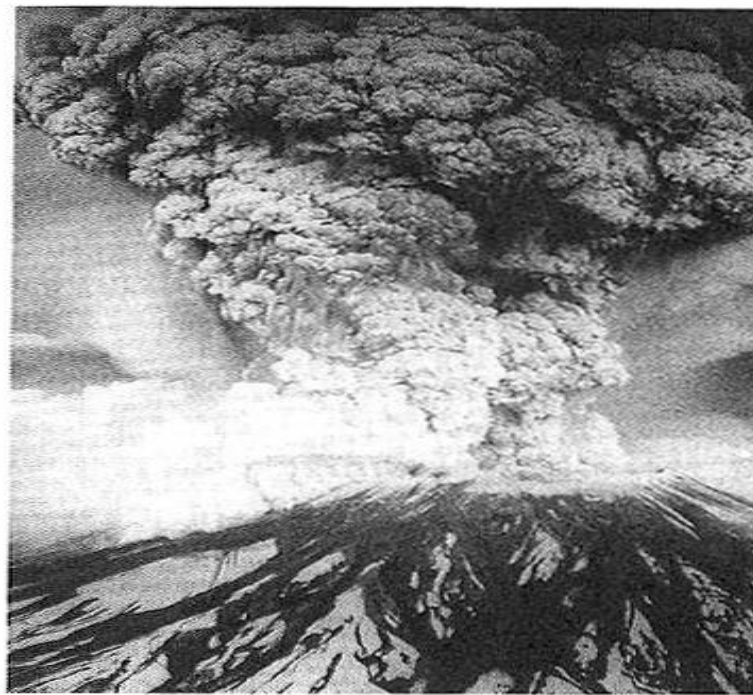
**FIGURE 1.2** (a) Granite cutting. (b) SEM photograph of quartz particles. Magnification 2650 $\times$ .



**FIGURE 1.3** (a) Arc welding. (b) SEM photograph of iron-oxide particles. Magnification 2300 $\times$ .



**FIGURE 1.4** (a) Removal of asbestos pipe covering. (b) SEM photograph of asbestos fibers. Magnification 1250 $\times$ .



**FIGURE 1.5** (a) Volcanic eruption of Mount St. Helens, May 1980. (b) Optical microscope photograph of volcanic ash. Magnification 125 $\times$ . USGS photograph by Austin Post. Reprinted from *Mount St. Helens: Five Years Later*. Courtesy of Eastern Washington University Press and W. C. McCrone and J. G. Delly, *The Particle Atlas*. Reprinted by permission from McCrone Research Institute.

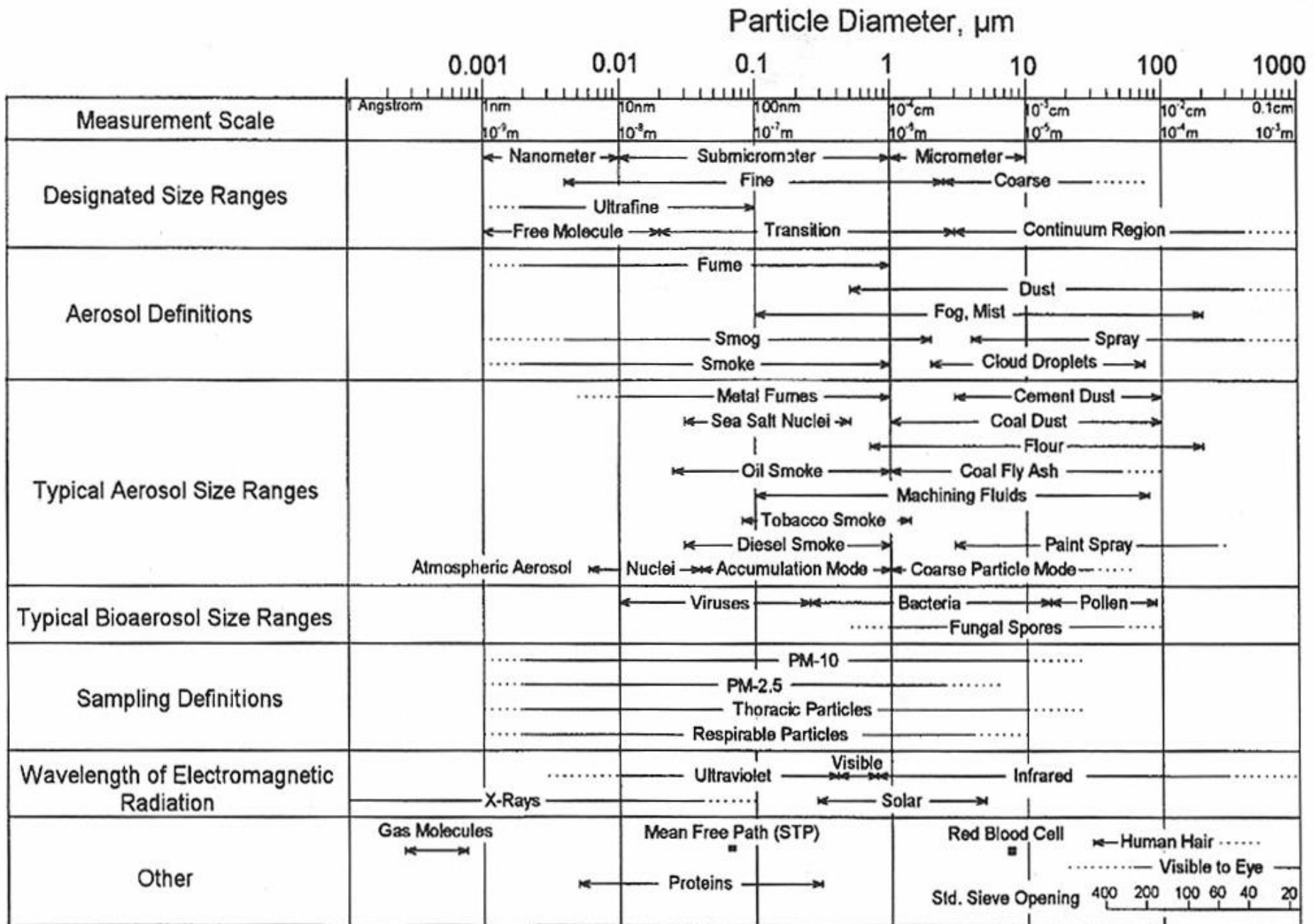


FIGURE 1.6 Particle size ranges and definitions for aerosols.



**TABLE 1.2 Examples of Mass Concentration Expressed in Parts per Million<sup>a</sup>**

	Mass Concentration, Mass/Volume (mg/m <sup>3</sup> )	Parts per Million, Volume/Volume (ppm)	Parts per Million, Mass/Mass (ppm)
U.S. PM-10, annual average	0.05	$5 \times 10^{-5}$	0.04
Threshold limit value for nuisance dusts (Particulates not otherwise classified)	10	0.01	8
Uncontrolled stack effluent (typical)	10,000	10	8,000

<sup>a</sup>Standard-density spheres.

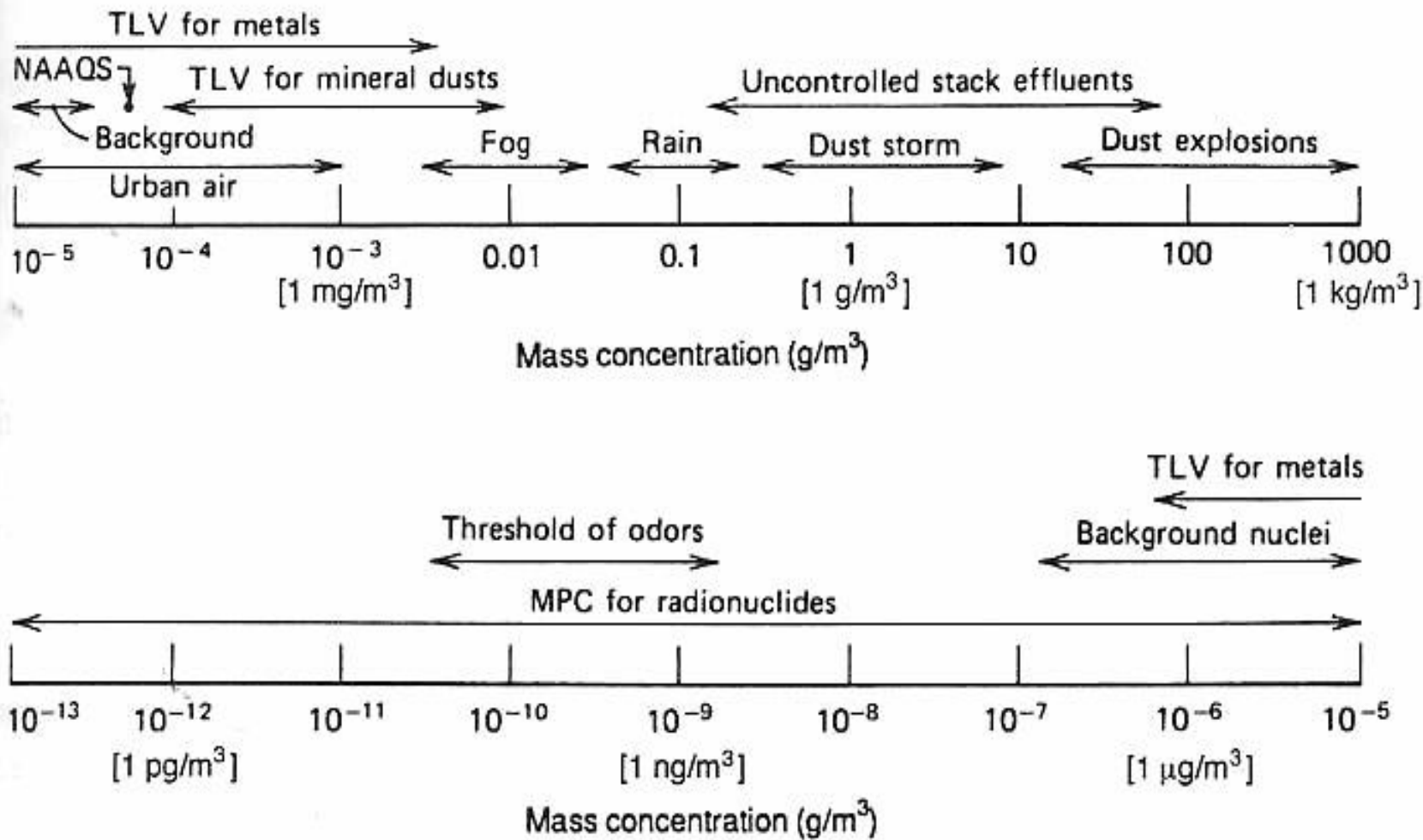


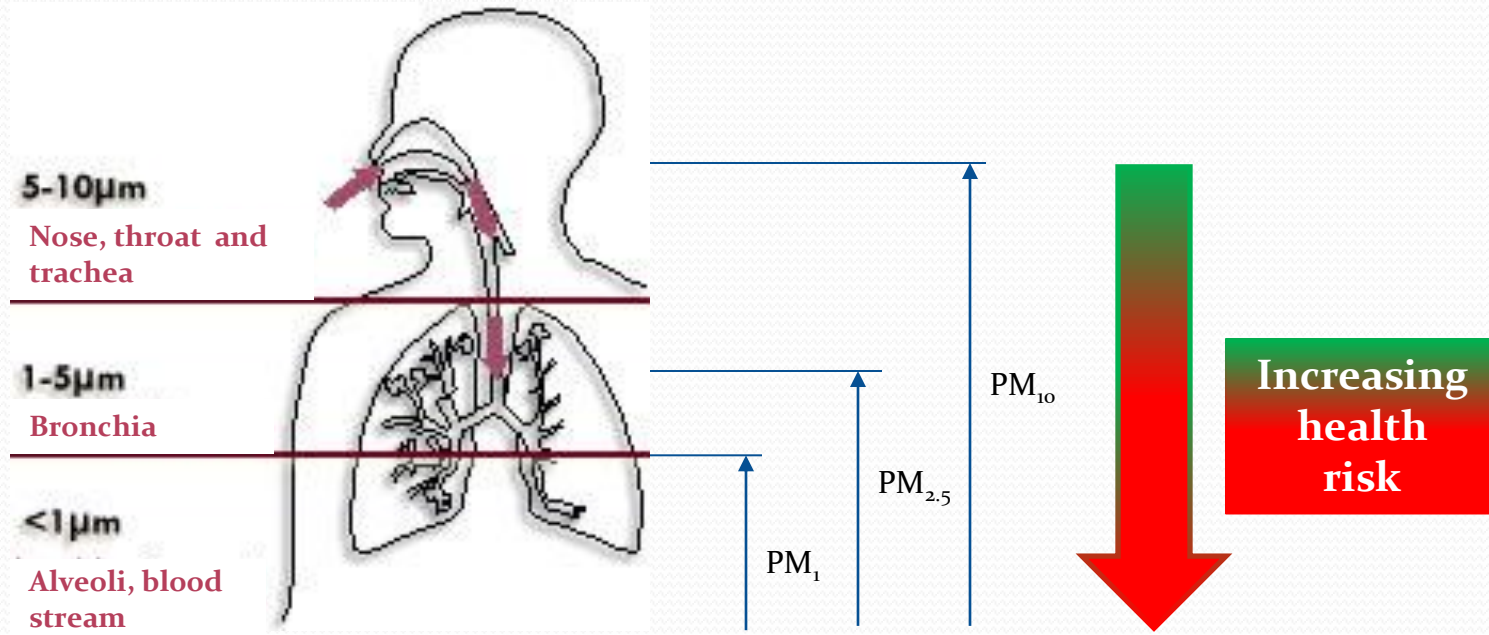
FIGURE 1.7 Range of aerosol concentration.

# PM<sub>X</sub>

(X = 10, 2.5, 1)

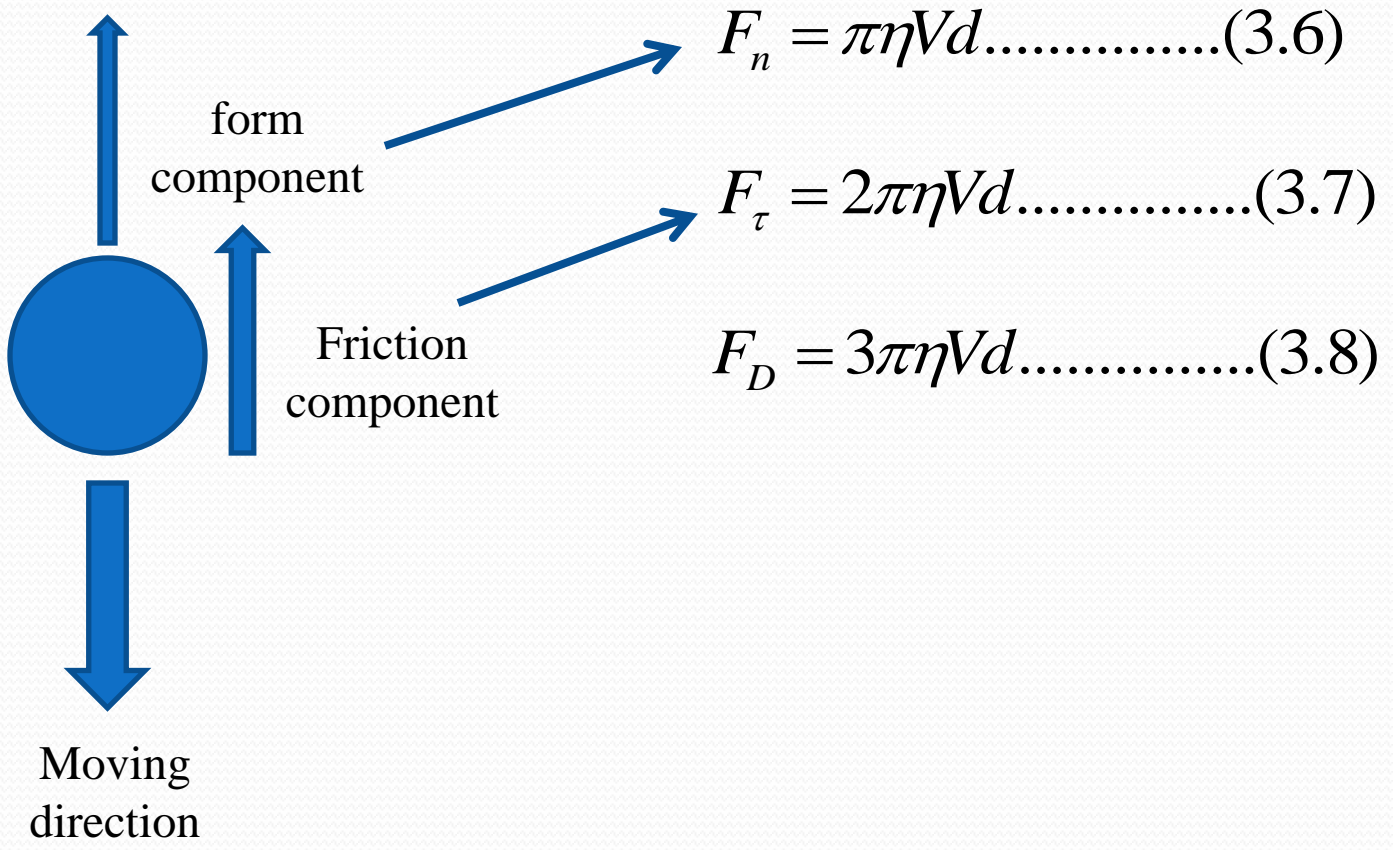
- PM<sub>X</sub> are all particles with an *Aerodynamic Equivalent Diameter (AED)* of less than X μm.
- AED is the diameter of a “unit density sphere 1 kg/m<sup>3</sup>” that would have the identical settling velocity as the particle ...
- Within ISO16890 particle measurement is done using an optical particle counter (OPC)
  - This device is limited in measurable particle size
  - AED is not used
  - The particle size range used is from 0.1μm ~ 10μm

# The human respiratory system and respirable aerosols



- Particles below 10µm are inhalable
- The smaller the particle the deeper it will end up in our respiratory system
- Special concern for particles below 2.5 µm

# Particle in the Air



# Forces

$$F_D = 3\pi\eta Vd = C_D \frac{\pi}{8} \rho_g V^2 d^2 \quad \text{for } \text{Re} < 1 \dots \dots \dots (3.9)$$

$$C_D = \frac{24\eta}{\rho_g Vd} = \frac{24}{\text{Re}} \dots \dots \dots (3.10)$$

- $\eta$  Air viscosity ( $1.81 \cdot 10^{-5} \text{ N} \cdot \text{s/m}^2$ )
- $V$  Particle Speed (m/s)
- $d$  Particle Diameter (m)
- $\rho_g$  Air density ( $\sim 1.20 \text{ kg/m}^3$ )

# Terminal Settling Velocity( $V_{TS}$ )

- Gravitational force =  $F_G$
- Air Drag Force  $F_D$
- Equal Force on particle:  $F_G = F_D$

$$F_D = F_G = mg \dots \dots \dots (3.11)$$

$$3\pi\eta Vd = \frac{(\rho_P - \rho_g)\pi d^3 g}{6} \dots \dots \dots (3.12)$$

$$V_{TS} = \frac{\rho_P d^2 g}{18\eta}, \quad \text{for } d > 1 \mu\text{m and } Re < 1.0 \dots \dots \dots (3.13)$$

# Particle Slips

- When particle is smaller than 1  $\mu\text{m}$ ,  $F_D$  will reduce

$$F_D = \frac{3\pi\eta Vd}{C_C} \dots\dots\dots(3.18)$$

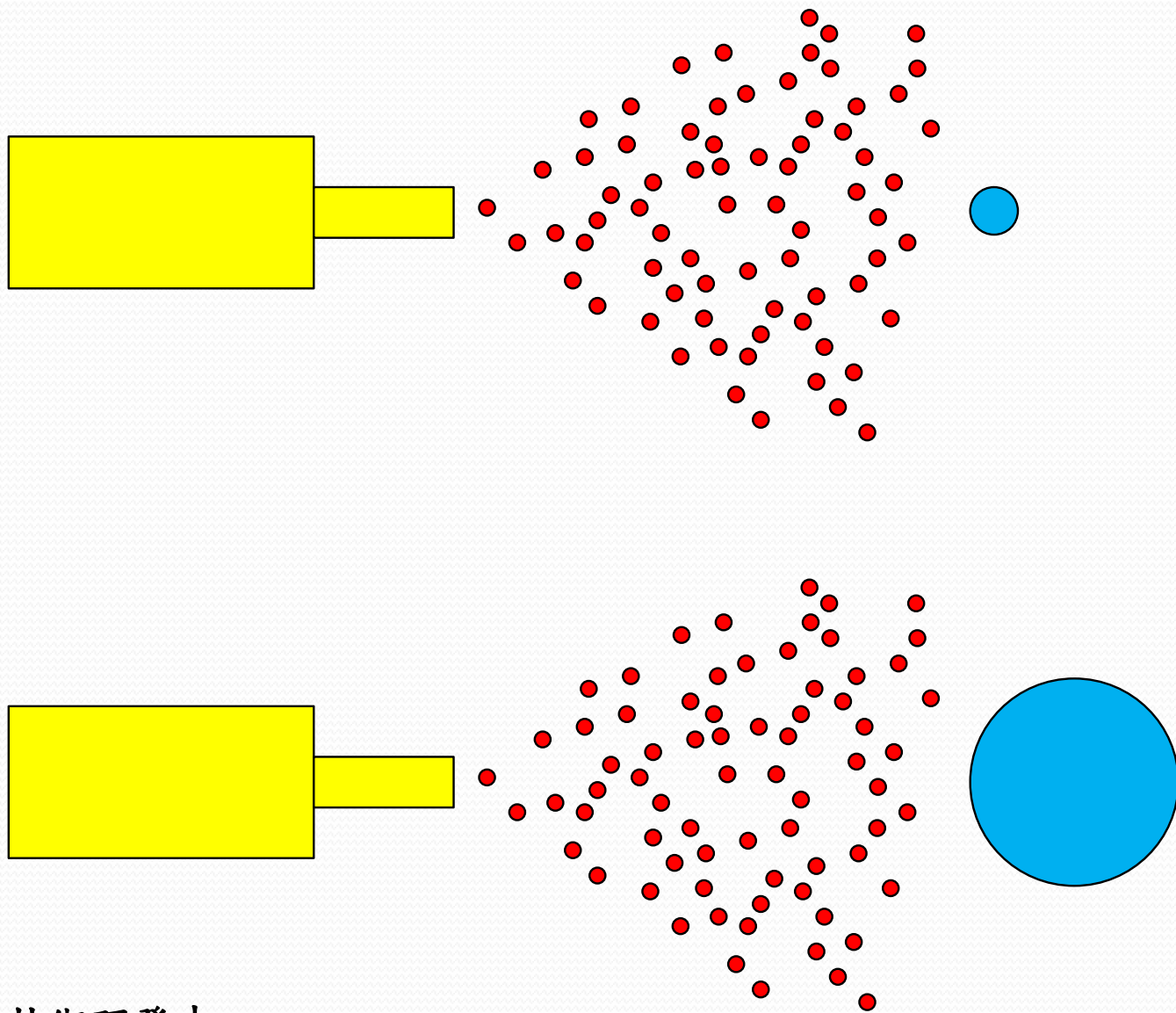
$$C_C = 1 + \frac{2.52\lambda}{d} \dots\dots\dots(3.19)$$

$$V_{TS} = \frac{\rho_P d^2 g C_C}{18\eta} \text{ for } \text{Re} < 1.0 \dots\dots\dots(3.21)$$

- $\lambda$  Mean Free Path (air: 0.066  $\mu\text{m}$ )

- For 0.1  $\mu\text{m}$  < d  $\leq$  1  $\mu\text{m}$



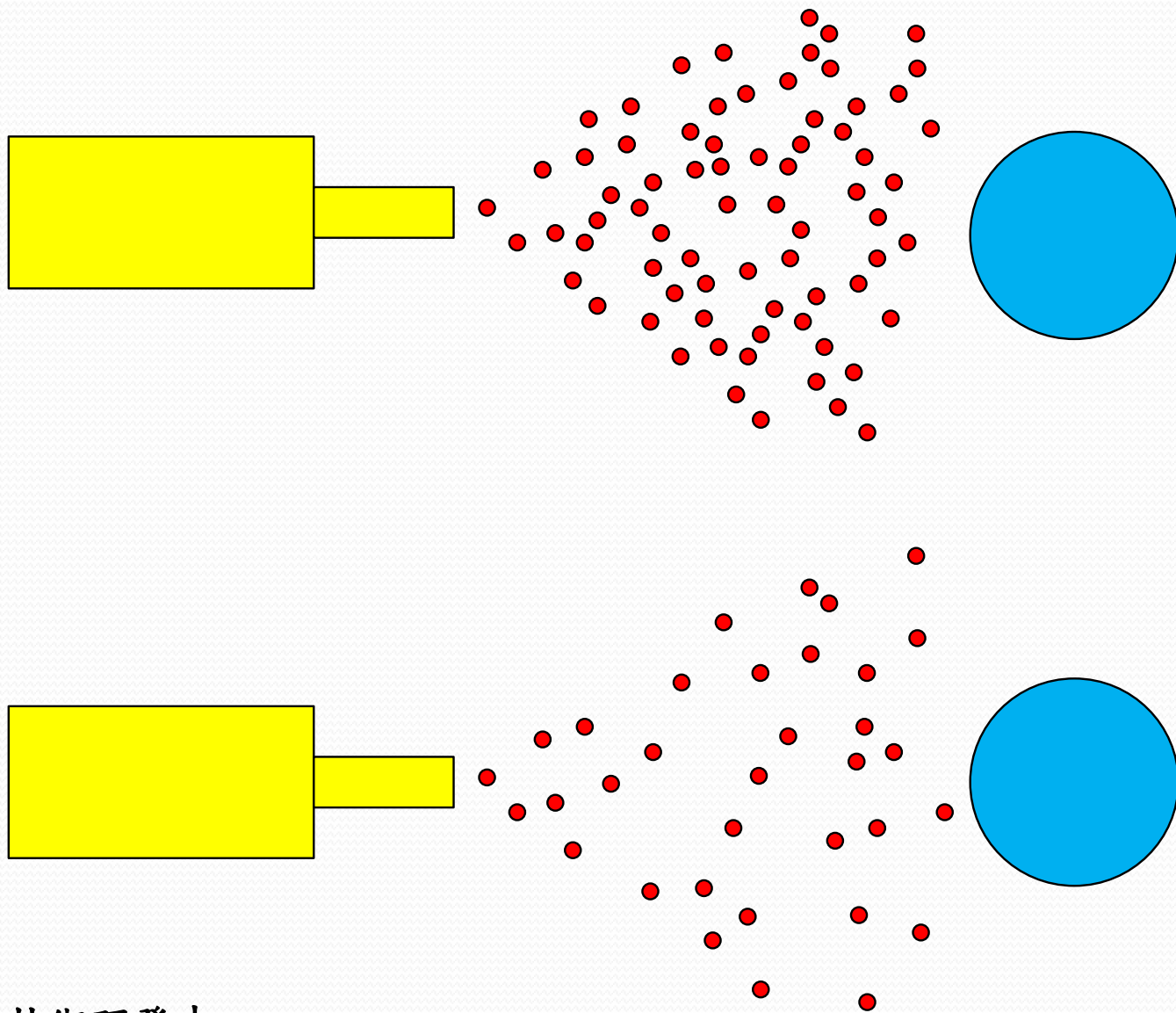


# Pressure reduces

- Air Pressure reduce =>  $F_D$  also reduce ◦

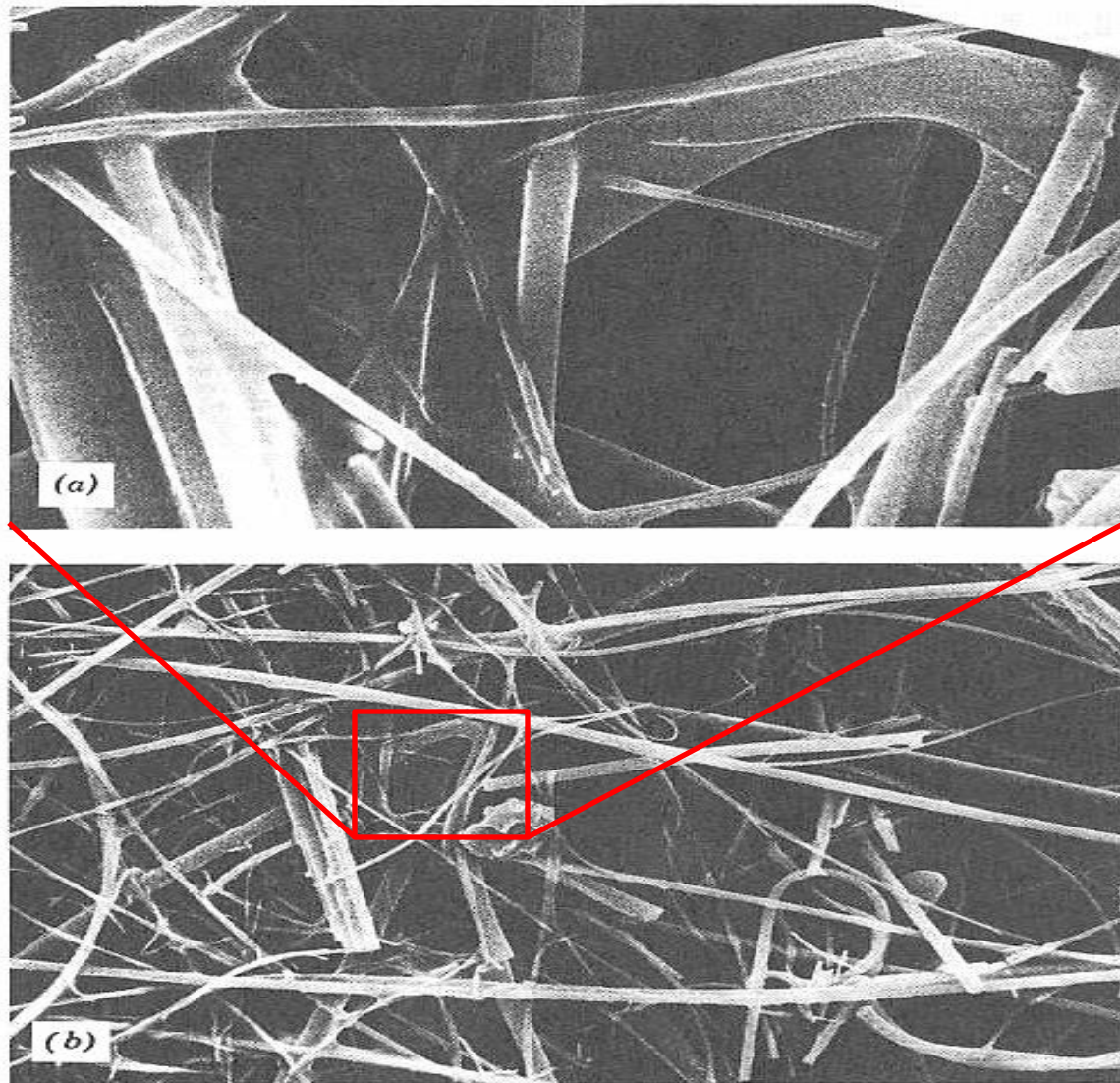
$$C_c = 1 + \frac{1}{Pd} [15.60 + 7.00 \exp(-0.059 Pd)] \dots \dots \dots (3.22)$$

- P Absolute Pressure(kPa)
- d Particle diameter( $\mu\text{m}$ )



# Particle Filter

# Fiber



**FIGURE 9.1** Scanning electron microscope photograph of a high-efficiency glass fiber filter. Magnification of (a) 4150 $\times$  and (b) 800 $\times$ .

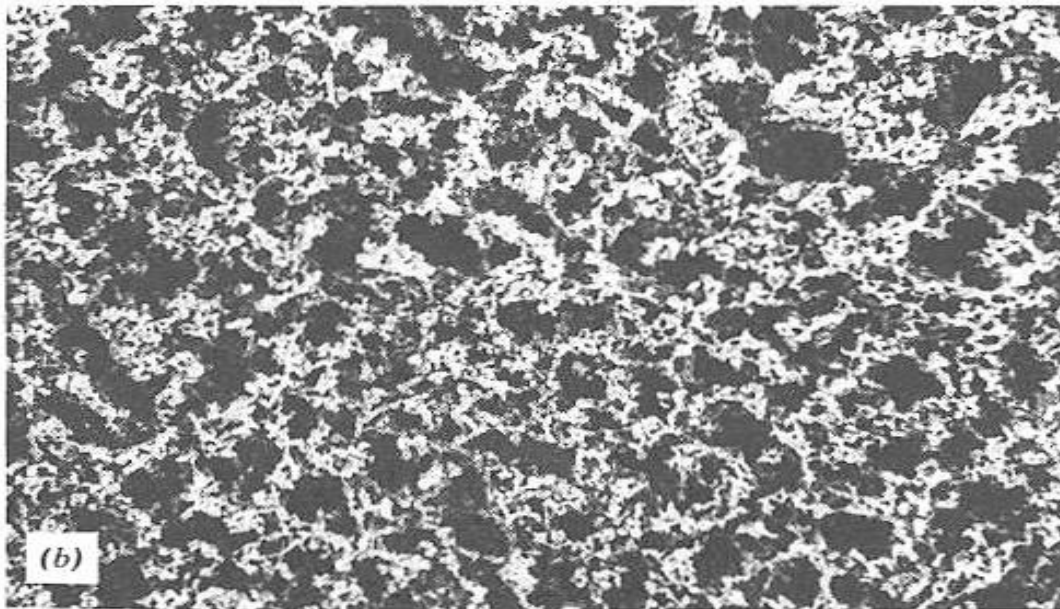
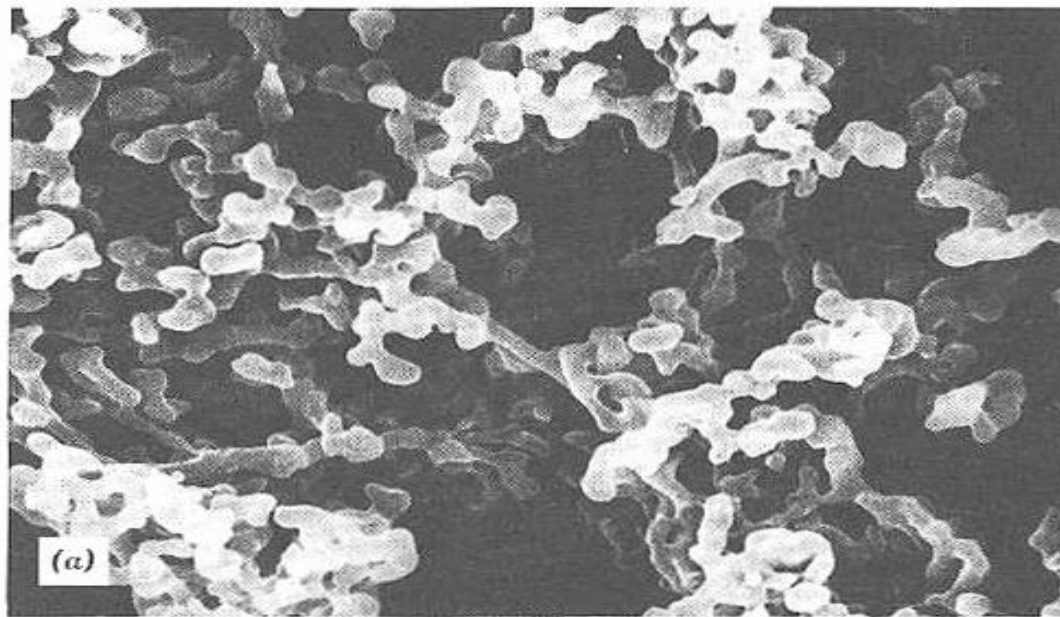
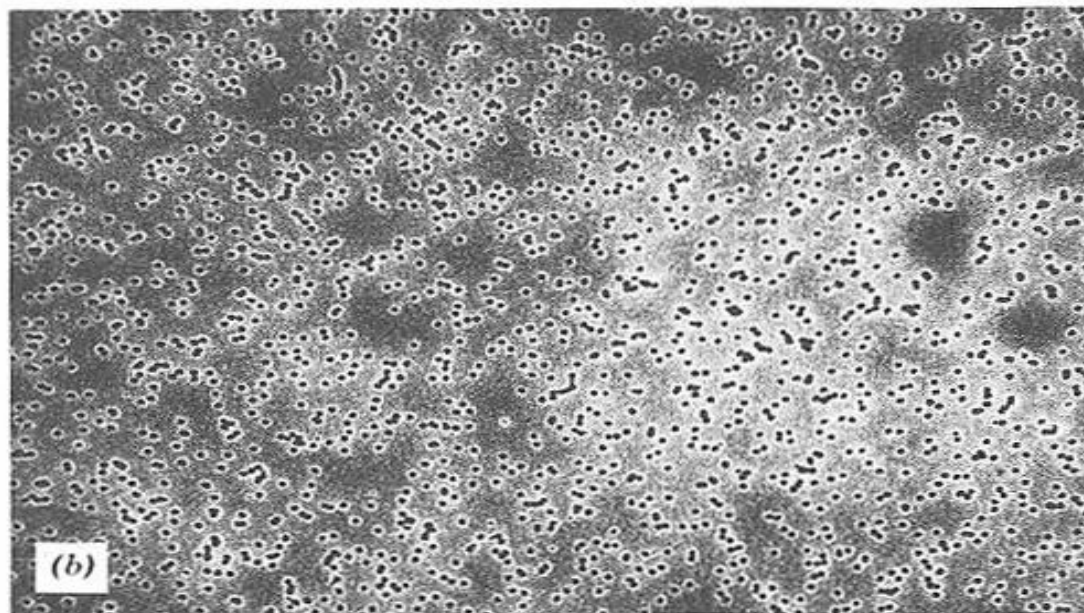
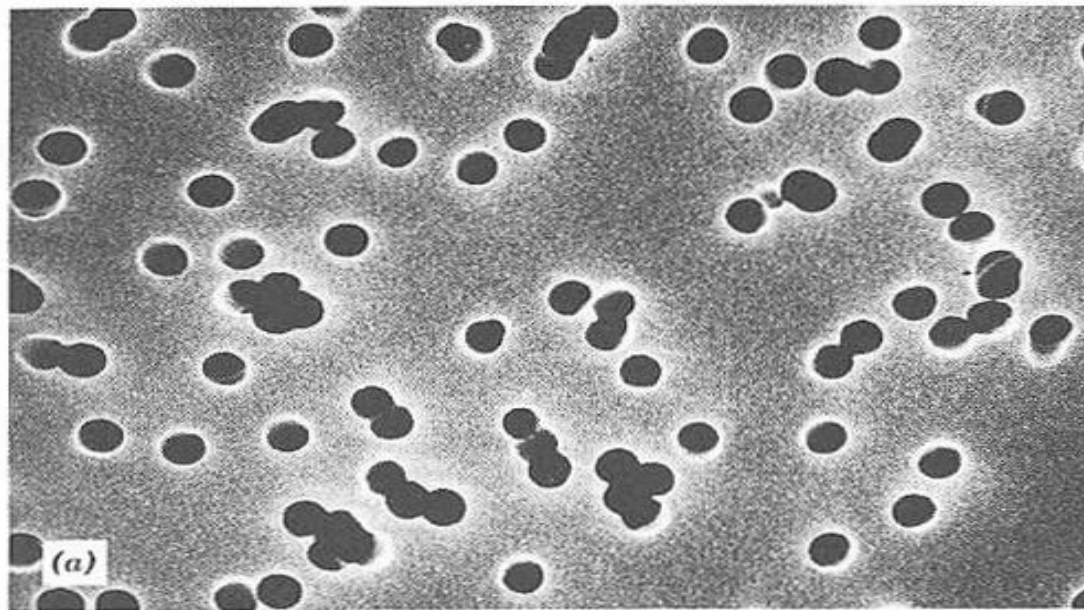
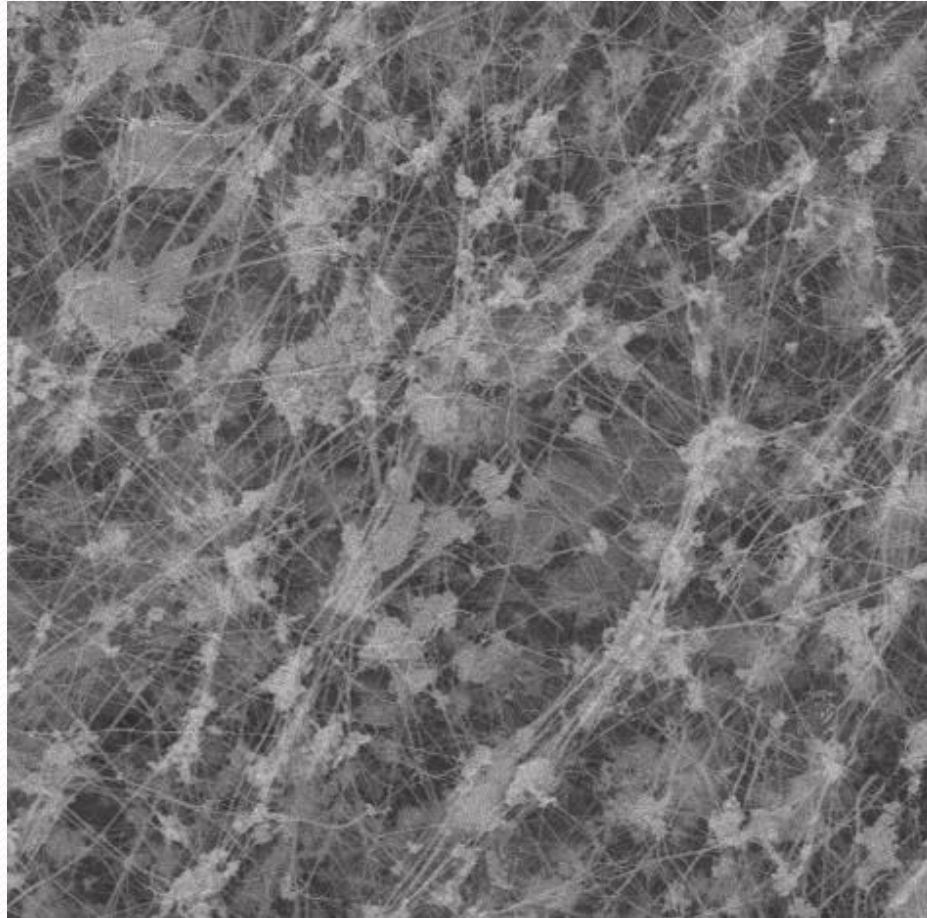


FIGURE 9.2 Scanning electron microscope photograph of a cellulose ester porous membrane filter with a pore size of 0.8  $\mu\text{m}$ . Magnification of (a) 4150 $\times$  and (b) 800 $\times$ .



**FIGURE 9.3** Scanning electron microscope photograph of a capillary pore membrane filter with a pore size of  $0.8\ \mu\text{m}$ . Magnification of (a)  $4150\times$  and (b)  $800\times$ .

# e-PTFE filter





# Efficiency & Penetration

$$E = \frac{N_{in} - N_{out}}{N_{in}} \dots\dots\dots(9.1) \quad P = \frac{N_{out}}{N_{in}} = 1 - E \dots\dots\dots(9.4)$$

In= 10000, out=100, P=100/10000

P=1% => Efficiency =99%

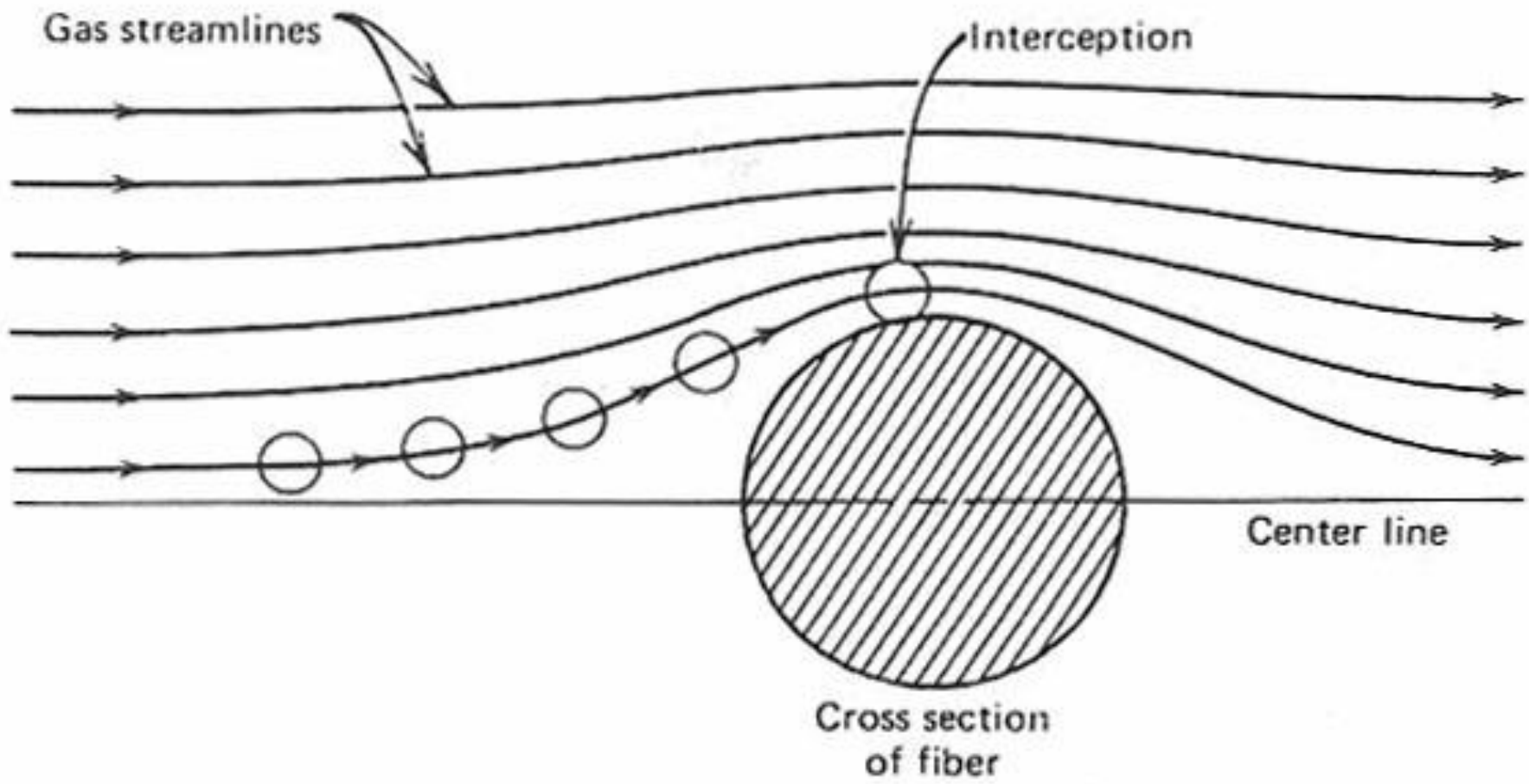
$$E_m = \frac{C_{in} - C_{out}}{C_{in}} \dots\dots\dots(9.2) \quad P_m = \frac{C_{out}}{C_{in}} = 1 - E_m \dots\dots\dots(9.3)$$

In= 10000#/m<sup>3</sup>, out=100#/m<sup>3</sup>, P=100/10000

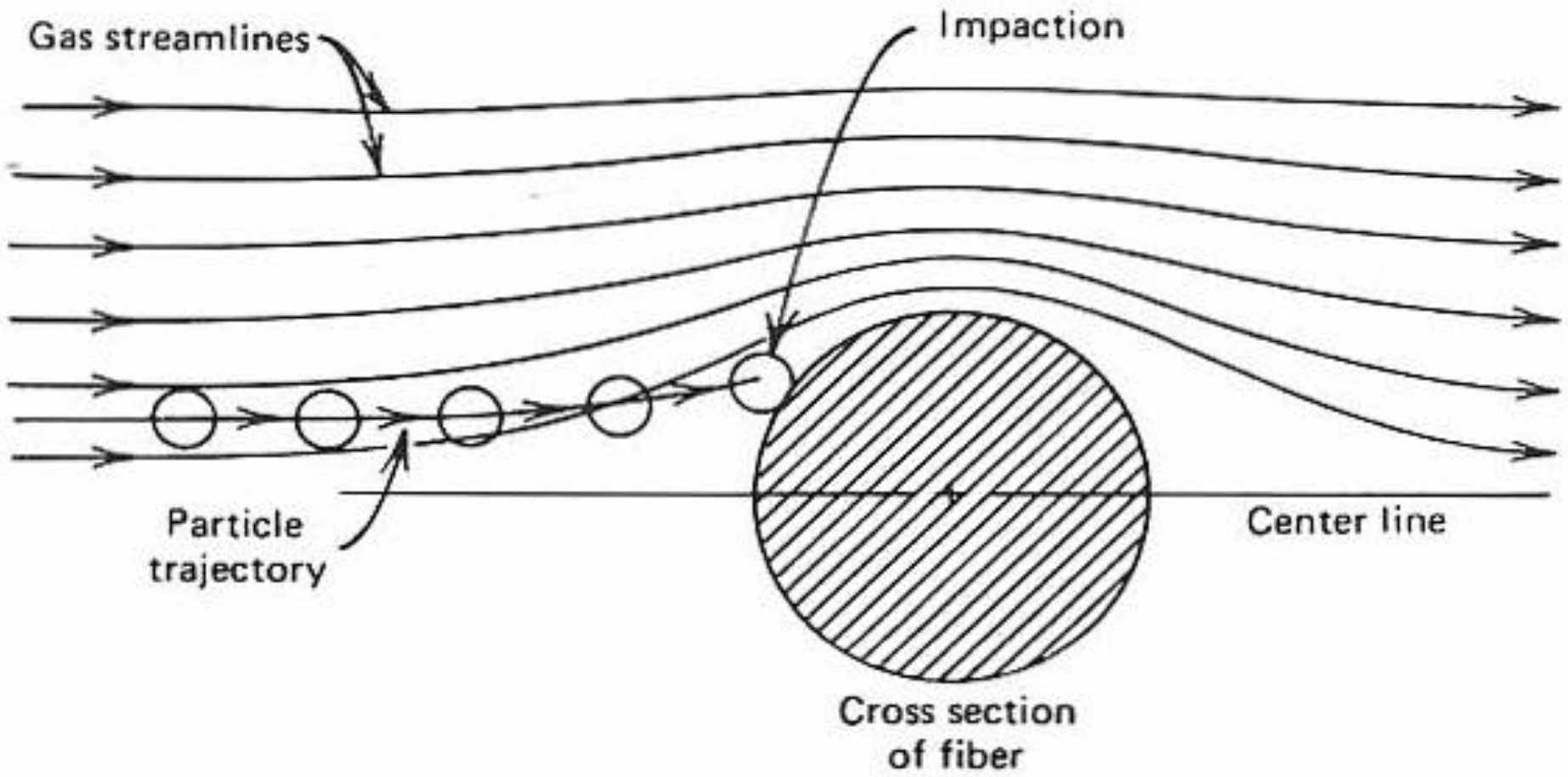
P=1% => Efficiency =99%

There are five basic mechanisms by which an particle can be deposited onto a fiber in a filter.

- 1 Interception
- 2 Inertial impaction
- 3 Diffusion
- 4 Gravitational settling
- 5 Electrostatic attraction



**FIGURE 9.5** Single-fiber collection by interception.



**FIGURE 9.6** Single-fiber collection by impaction.

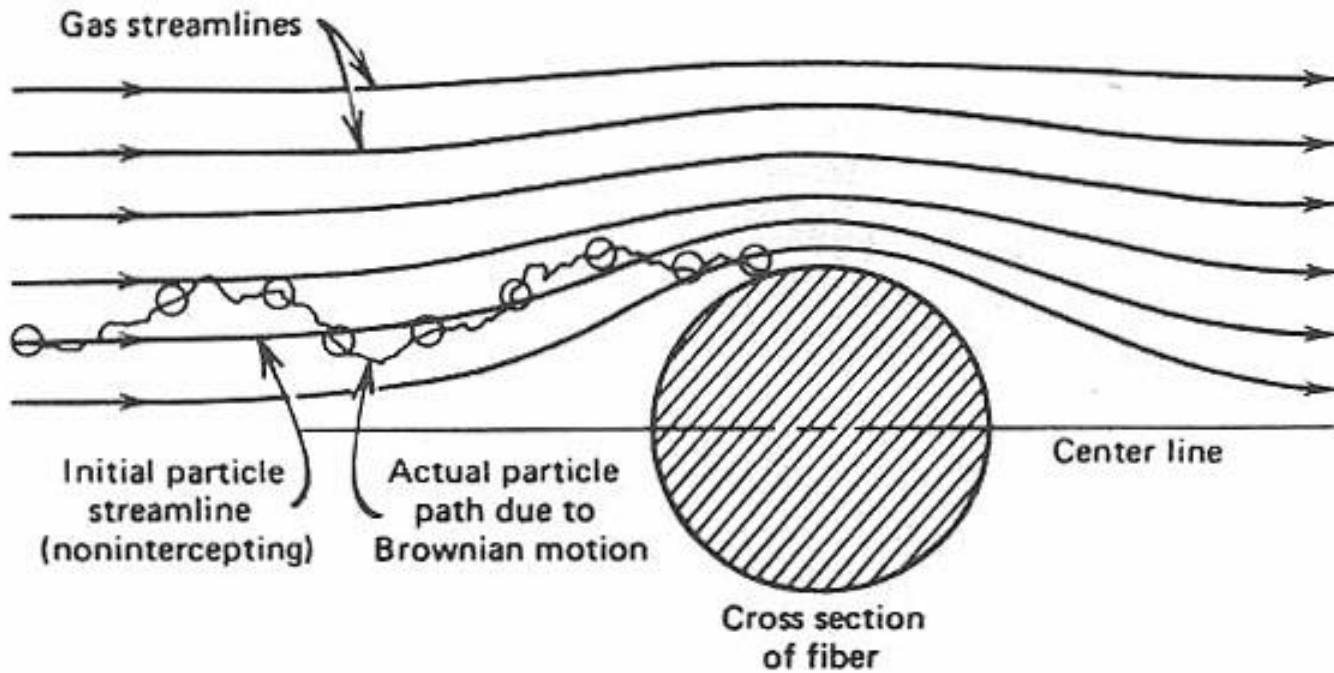


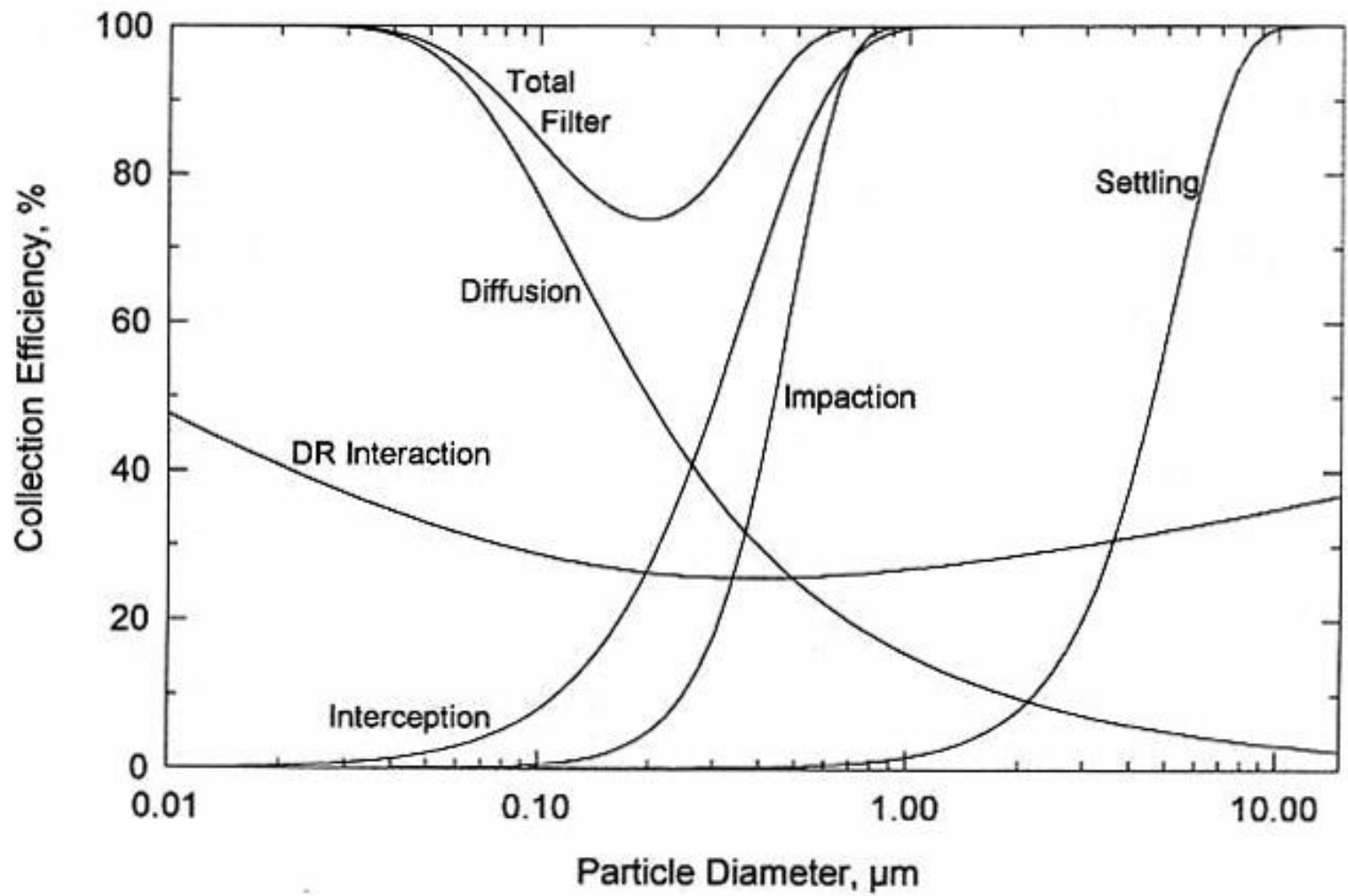
FIGURE 9.7 Single-fiber collection by diffusion.

**TABLE 9.2 Single-Fiber and Total Efficiency for a Filter Having  $t = 1$  mm,  $\alpha = 0.05$ ,  $d_f = 2 \mu\text{m}$ , and  $U_0 = 0.1$  m/s [10 cm/s]**

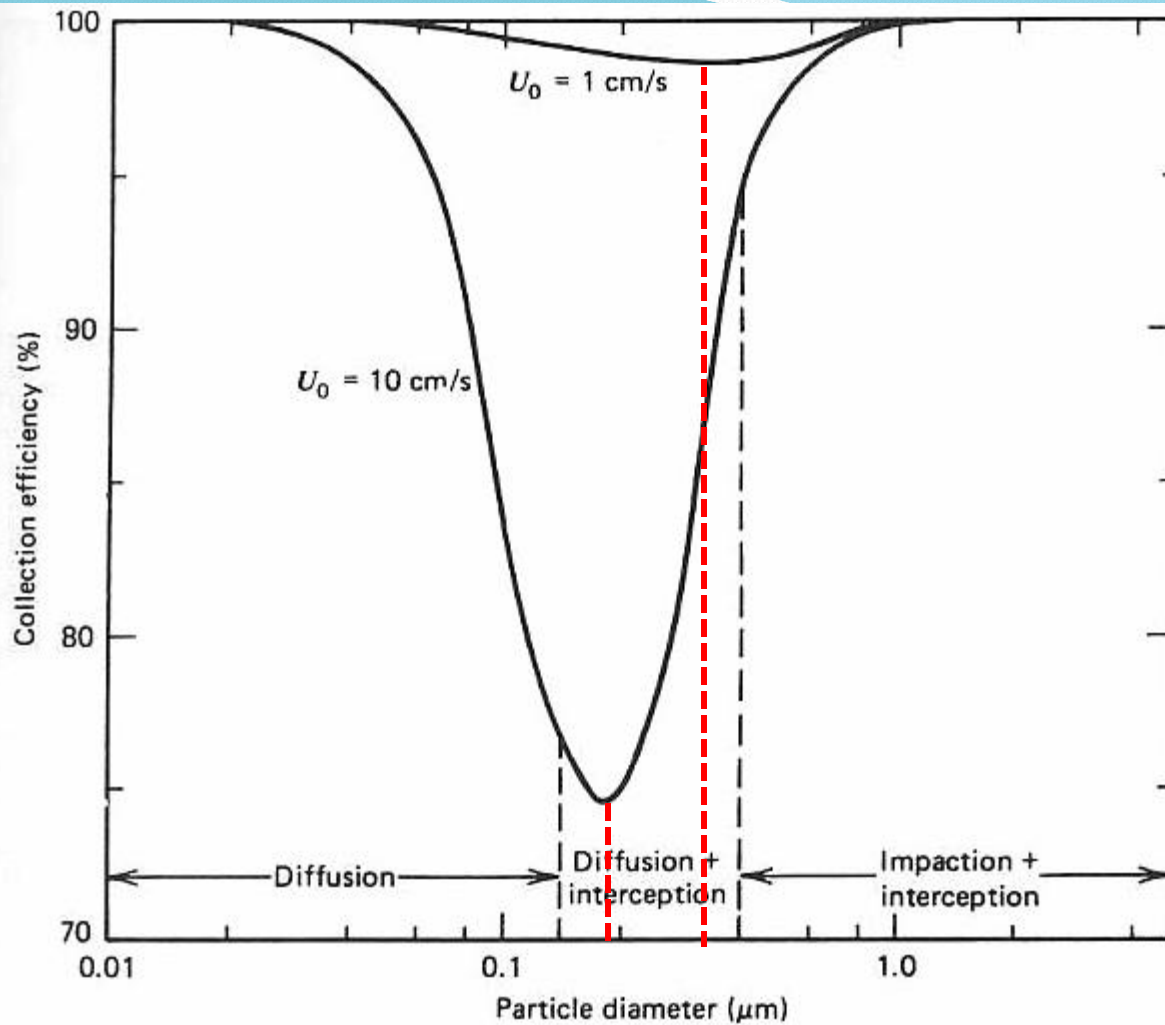
Particle Diameter ( $\mu\text{m}$ )	Single-Fiber Efficiency <sup>a</sup>						Overall Filter Efficiency <sup>b</sup> (%)
	$E_R$	$E_I$	$E_D$	$E_{DR}$	$E_G$	$E_\Sigma$	
0.01	0.000	0.000	0.840	0.020	0.000	0.861	100.0
0.02	0.000	0.000	0.339	0.016	0.000	0.356	100.0
0.05	0.001	0.000	0.106	0.013	0.000	0.119	97.7
0.1	0.003	0.000	0.046	0.011	0.000	0.059	84.9
0.2	0.010	0.002	0.021	0.010	0.000	0.043	74.3
0.5	0.055	0.034	0.009	0.009	0.000	0.108	96.8
1.0	0.183	0.238	0.005	0.010	0.001	0.437	100.0
2.0	0.550	0.887	0.003	0.011	0.003	1.454	100.0
5.0	1.965	3.500	0.002	0.012	0.027	3.500	100.0
10.0	4.585	6.000	0.001	0.014	0.183	6.000	100.0

<sup>a</sup>Calculated by Eq. 9.33b, assuming spheres of standard density at standard conditions.

<sup>b</sup>Calculated by Eq. 9.19.

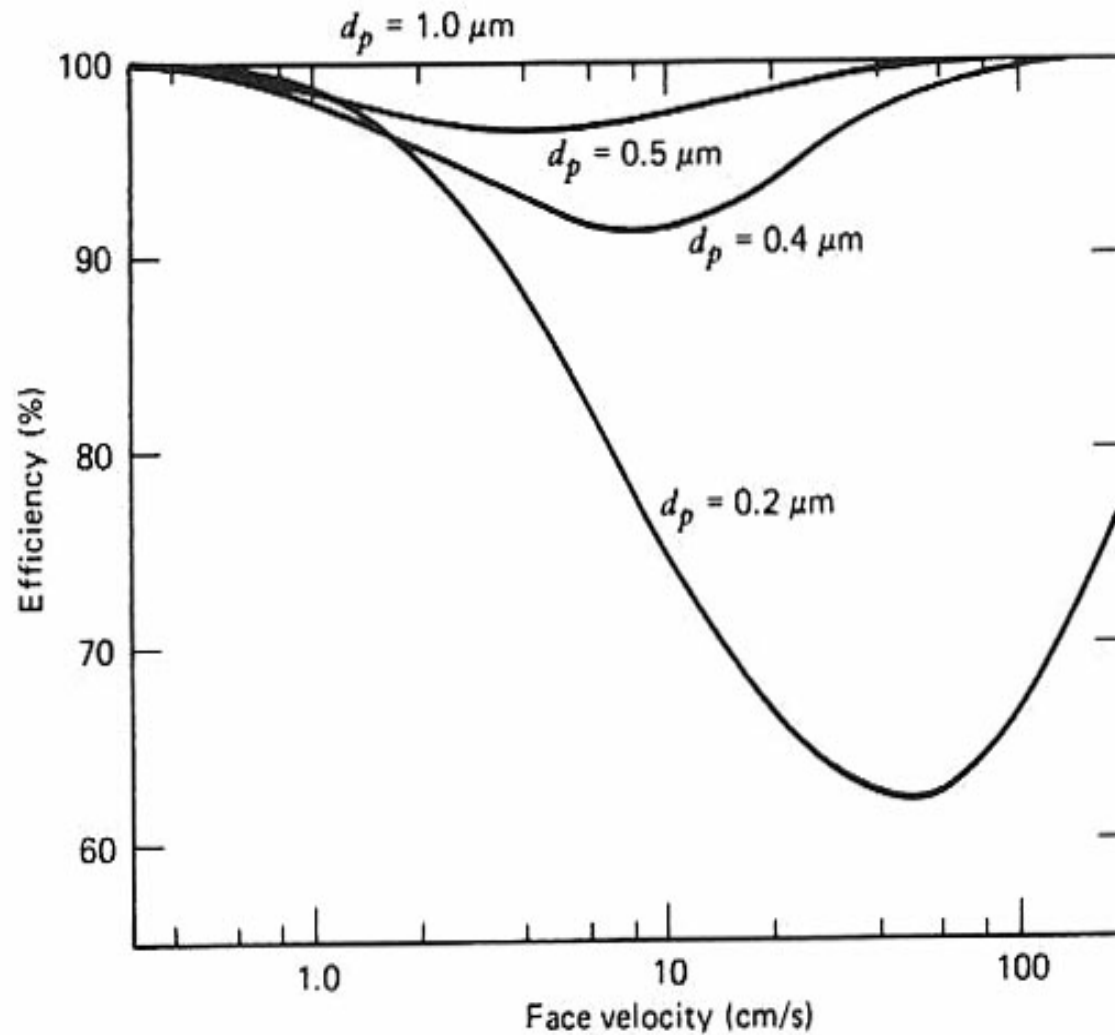


**FIGURE 9.8** Filter efficiency for individual single-fiber mechanisms and total efficiency;  $t = 1 \text{ mm}$ ,  $\alpha = 0.05$ ,  $d_f = 2 \text{ } \mu\text{m}$ , and  $U_0 = 0.10 \text{ m/s}$ . [10 cm/s].



**FIGURE 9.9** Filter efficiency versus particle size for face velocities of 0.01 and 0.1 m/s [1 and 10 cm/s];  $t = 1 \text{ mm}$ ,  $\alpha = 0.05$ , and  $d_f = 2 \mu\text{m}$ .





**FIGURE 9.10** Filter efficiency versus face velocity for particle diameters of 0.2, 0.4, 0.5, and 1  $\mu\text{m}$ ;  $t = 1 \text{ mm}$ ,  $\alpha = 0.05$ , and  $d_f = 2 \mu\text{m}$ .

# Filter types

Gas & Particle

# Filter category

- Particle size
  - Coarse, medium, Fine
  - Pre-filter, Mid-filter, High eff. filters(HEPA, ULPA)
- Molecular / Particle
  - Chemical filter, Fiber filters

# Particle Filter

# Classifications

- ISO-16890, ISO-29463
- EN-779, EN-1822
- ASHRAE 52.2

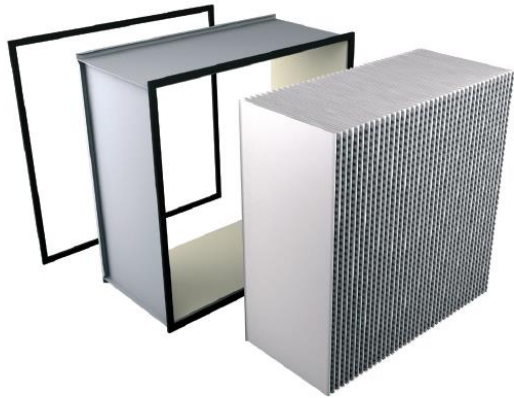
# EN1822 to EN779 to ASHRAE

EN1822: 2009 Classes	EN1822: 2009 Efficiency	EN779:2012 Classes		EN779: 2002 Classes	ASHRAE Standard 52.2 MERV	Approx. ASHRAE Standard 52.1 Values	
		Filter Grade	Discharged Initial Efficiency			Avg. Dust Spot Efficiency	Arrestance
U17	>99.999995%	n/a	n/a	n/a	n/a	n/a	n/a
U16	>99.99995%	n/a	n/a	n/a	n/a	n/a	n/a
U15	>99.9995%	n/a	n/a	n/a	n/a	n/a	n/a
H14	>99.995%	n/a	n/a	n/a	20	n/a	n/a
H13	>99.95%	n/a	n/a	n/a	19	n/a	n/a
E12	>99.5%	n/a	n/a	n/a	18	n/a	n/a
E11	>95%	n/a	n/a	n/a	17	n/a	n/a
E10	>85%	n/a	n/a	n/a	16	n/a	n/a
n/a	n/a	F9	>70%	F9	15	>95%	n/a
n/a	n/a	F8	>55%	F8	14	90% - 95%	>98%
n/a	n/a	F7	>35%	F7	13	80% - 90%	>98%
n/a	n/a	M6	<35%	F6	12	70% - 75%	>95%
n/a	n/a	M6	<35%	F6	11	60% - 65%	>95%
n/a	n/a	M5	n/a	F5	10	50% - 55%	>95%
n/a	n/a	G4	n/a	G4	9	40% - 45%	>90%
n/a	n/a	G4	n/a	G4	8	30% - 35%	>90%
n/a	n/a	G4	n/a	G4	7	25% - 30%	>90%
n/a	n/a	G3	n/a	G3	6	<20%	85% - 90%
n/a	n/a	G3	n/a	G3	5	<20%	80% - 85%
n/a	n/a	G2	n/a	G2	4	<20%	75% - 80%
n/a	n/a	G2	n/a	G2	3	<20%	70% - 75%
n/a	n/a	G2	n/a	G2	2	<20%	65% - 70%
n/a	n/a	G1	n/a	G1	1	<20%	50% - 65%

# Bag-Filter (G1~F9)



# Pleated Type Filter E10~U17



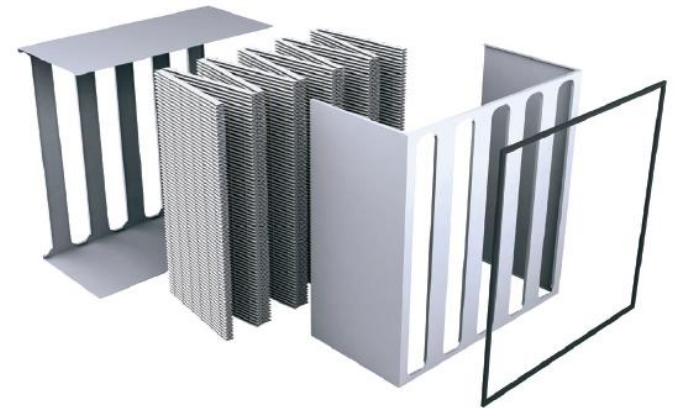
**Deep Pleat design**

**Mid Velocity**



**minipleat/closepleat  
design**

**Low Velocity**



**'V' bank design**

**High Velocity**



# Fiber-Glass HEPA filter

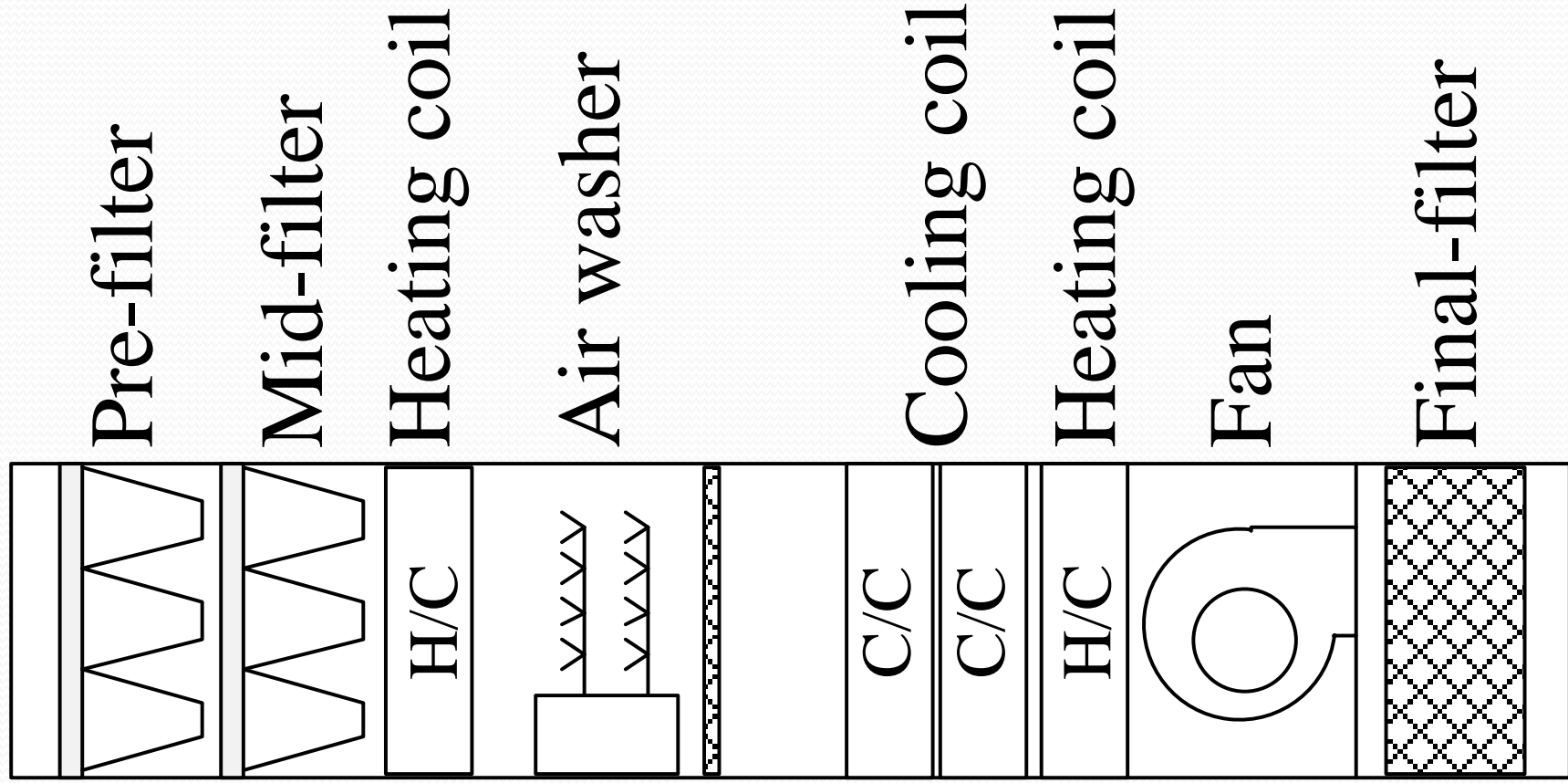


## During:

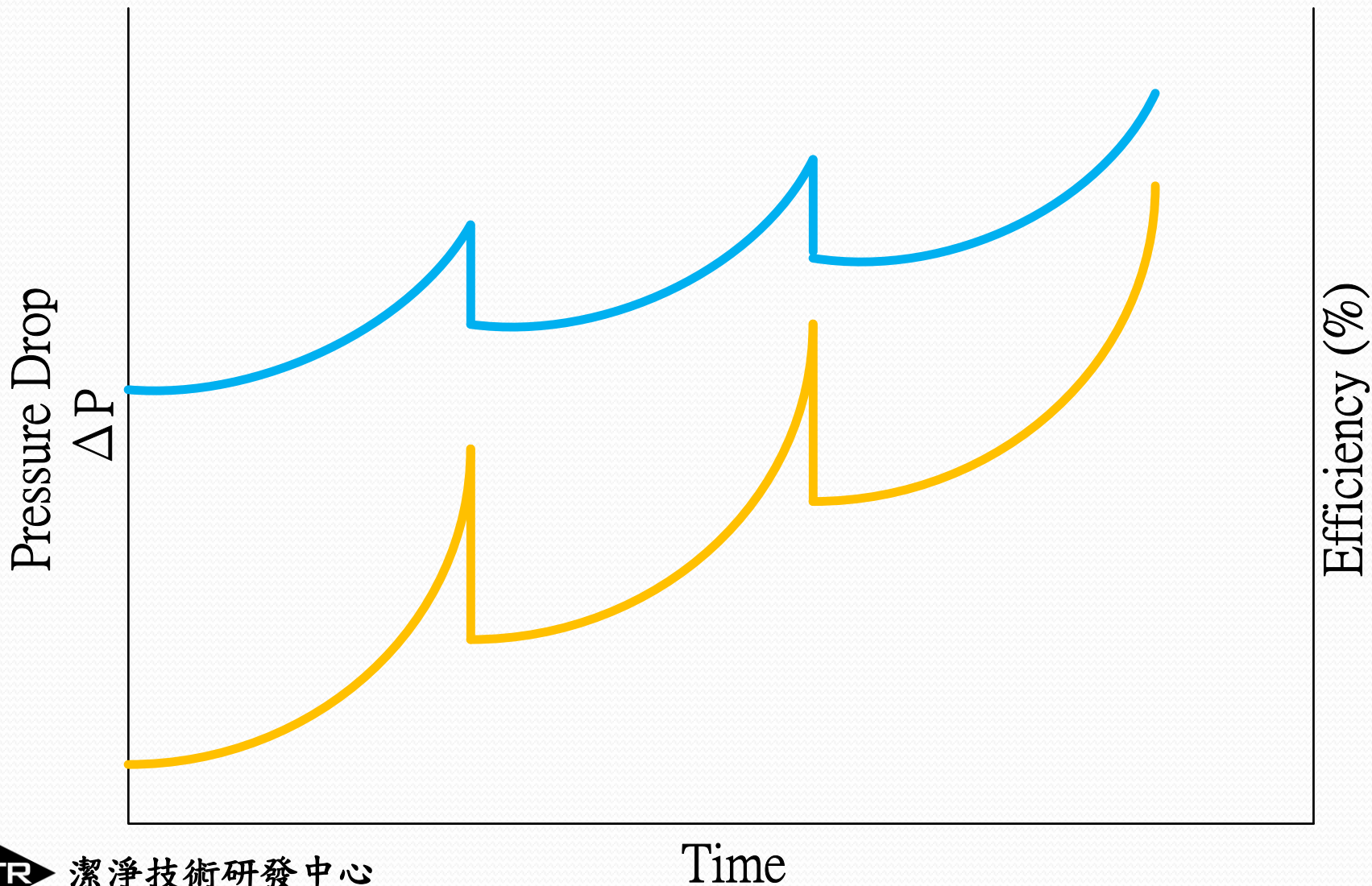
- ▶ filter installation
- ▶ filter validation
- ▶ cleaning of ceiling
- ▶ cleanroom modifications
- ▶ working activities in the cleanroom



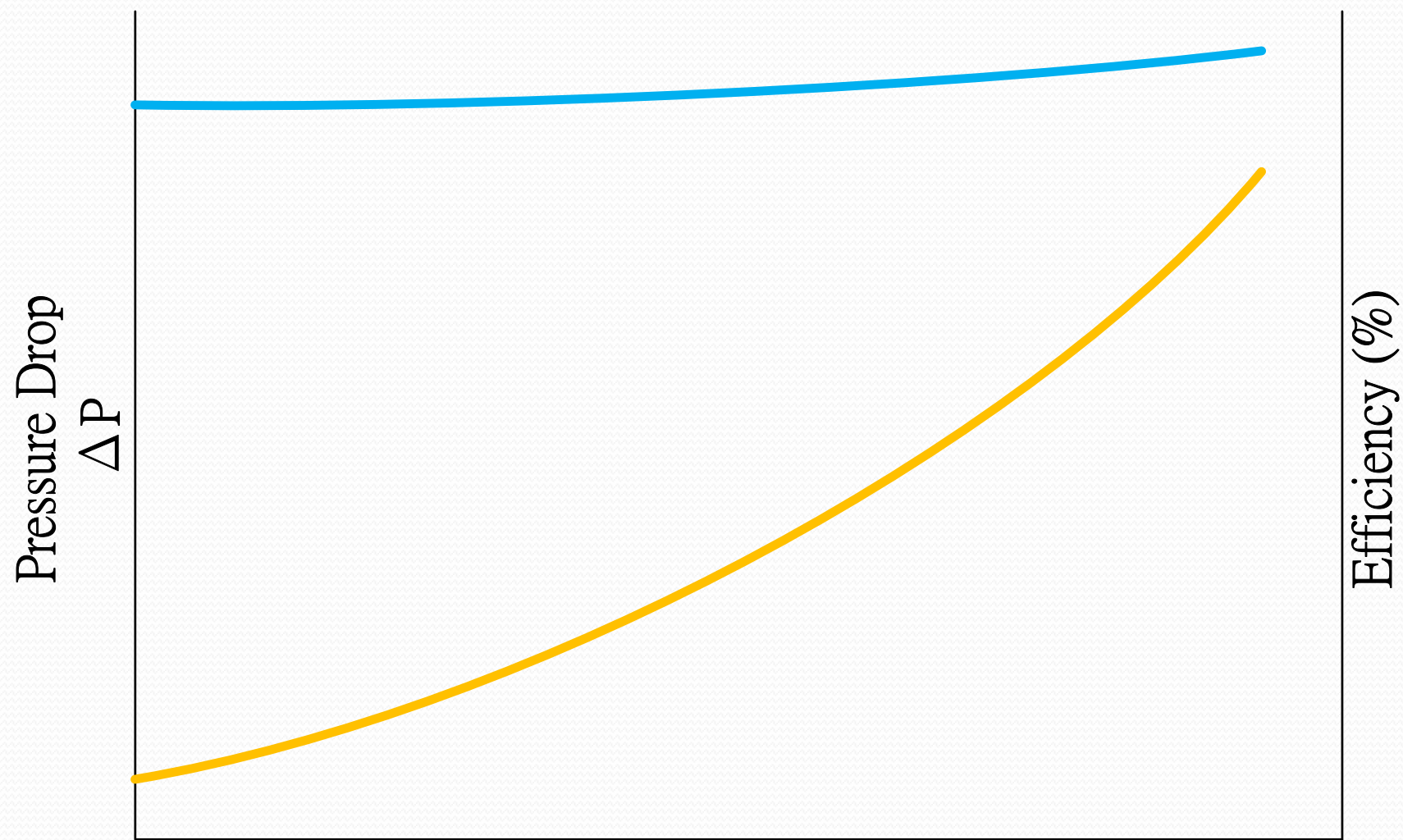
# Filter installation Locations



# Filter Pressure drop & Eff. (PF&MF)

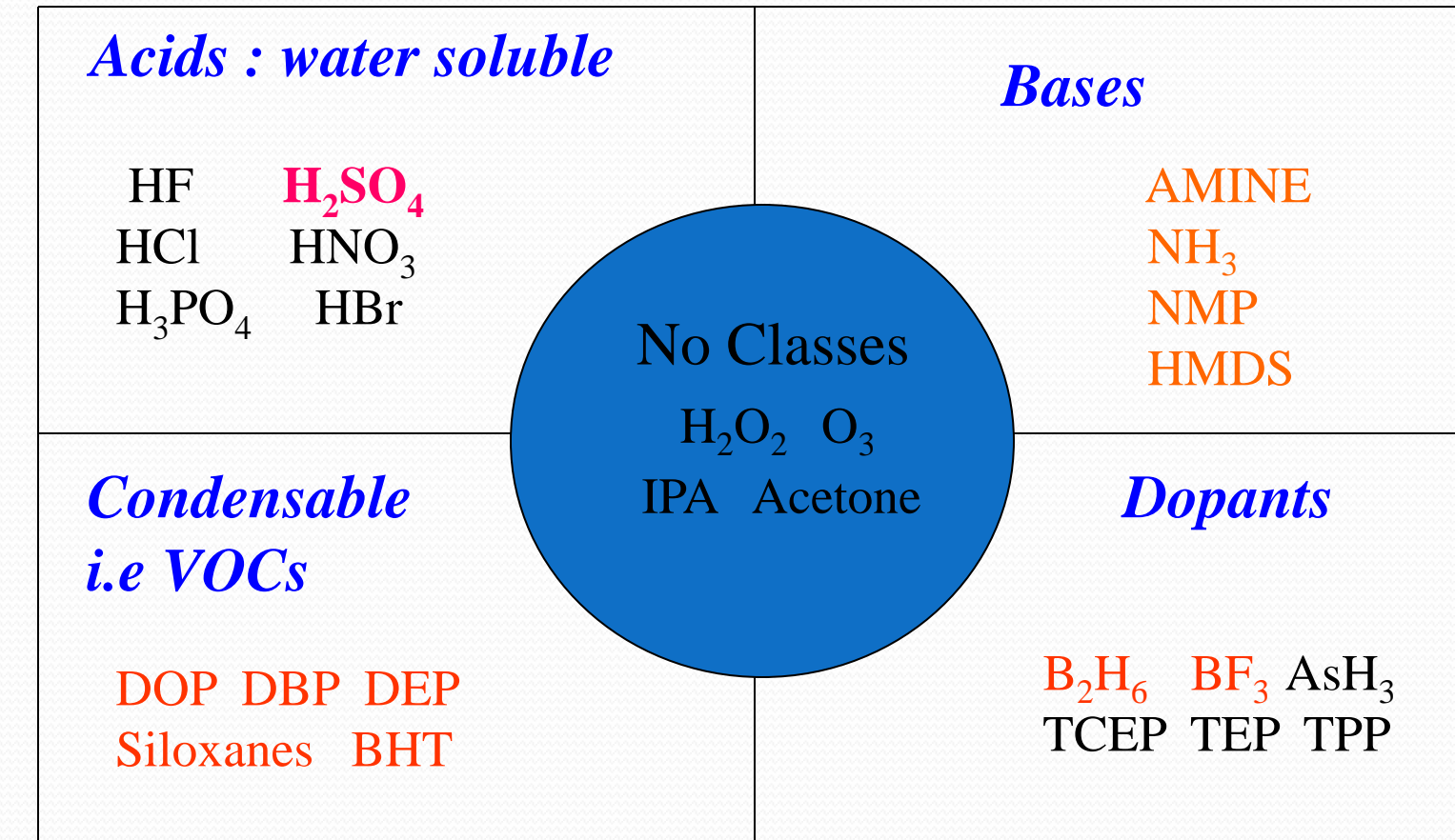


# Filter Pressure drop & Eff. (HEPA)



# Chemical Filter

# Classification of AMCs

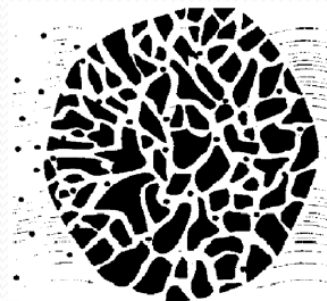


REF: SEMI Standard F21-95, 1996

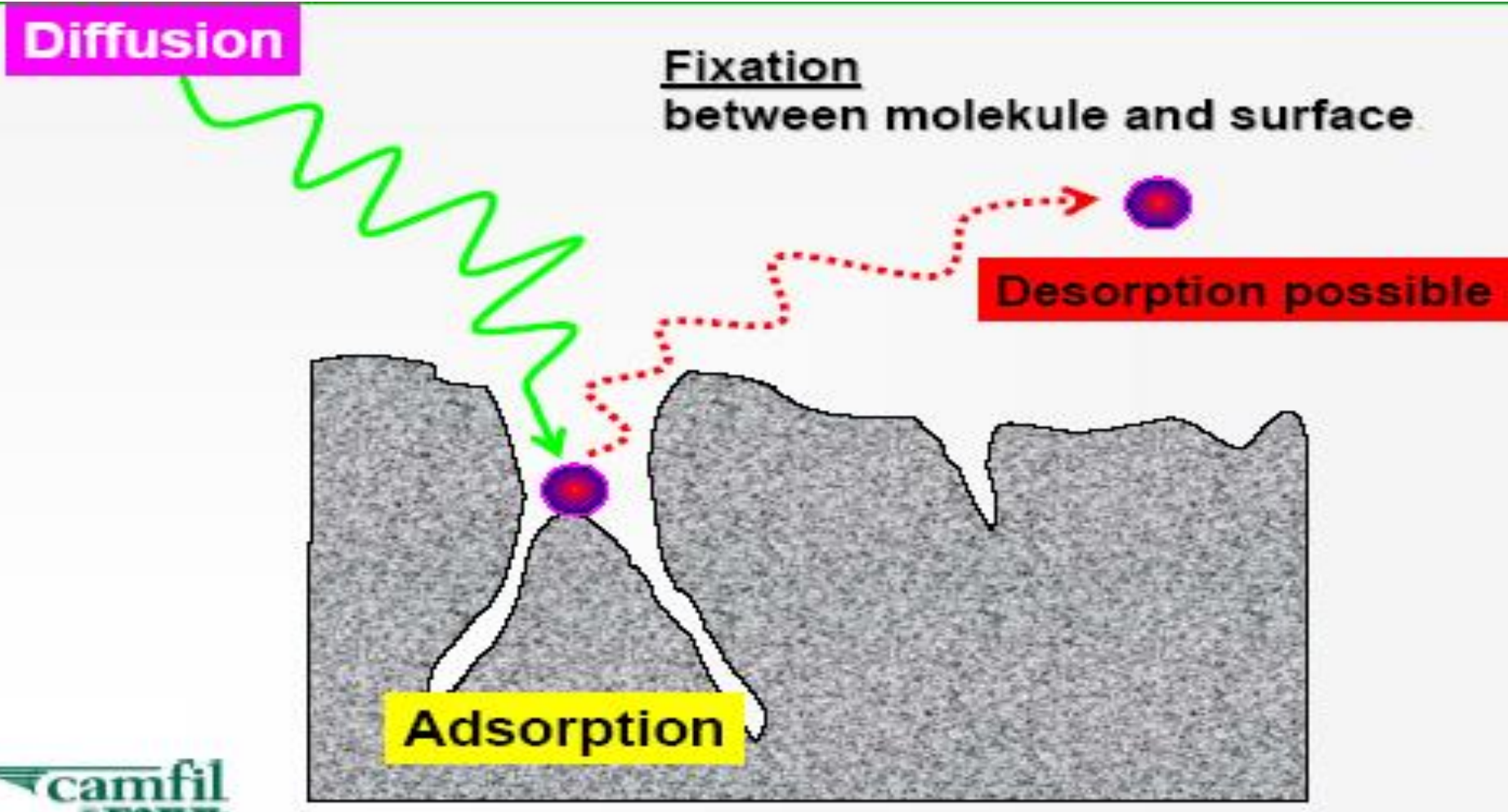
# Gas-Phase Air Filtration Principles

- **Adsorption**

- Most commonly involves the use of granular activated carbon (GAC) media.
- High surface area to volume ratio.
- Very good against most hydrocarbons, many aldehydes and organic acids, and nitrogen dioxide.
- Organic gases with more than 3 carbon atoms eg: Solvents, Benzine steams, Kerosene, Odours



# Gas-Phase Air Filtration Principles (cont.)

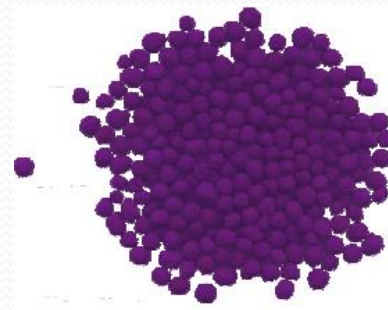
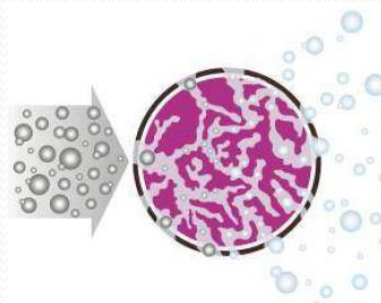




# Gas-Phase Air Filtration Principles (cont.)

- Chemisorption

- Most commonly involves permanganate impregnated alumina (PIA) media.
- Chemically converts contaminants to carbon dioxide, water, and non-toxic salts.
- Effective against oxides of sulfur, lower molecular weight aldehydes and organic acids, nitric oxide, and hydrogen sulfide.
- Anorganicalgases eg:–Acids (  $\text{SO}_2$ ,  $\text{NO}_x$ ,  $\text{H}_2\text{S}$ ), Ammonia ( $\text{NH}_3$ ), Formaldehyde, Nuclear Filter (eg. Methyl iodine), Mercury



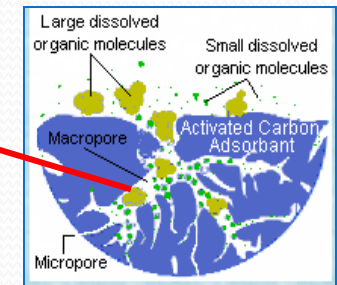
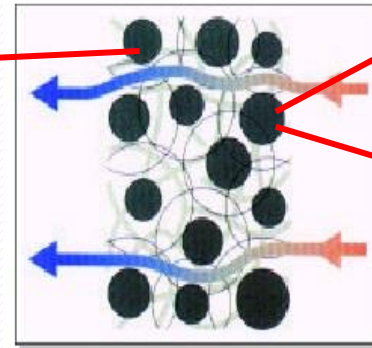
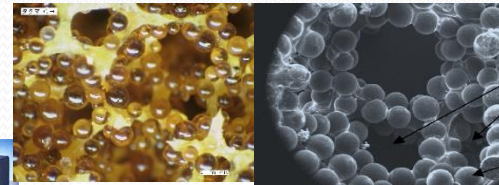
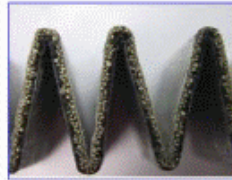
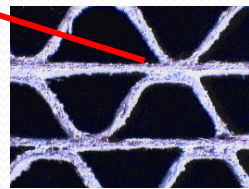
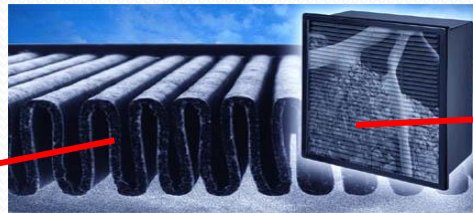
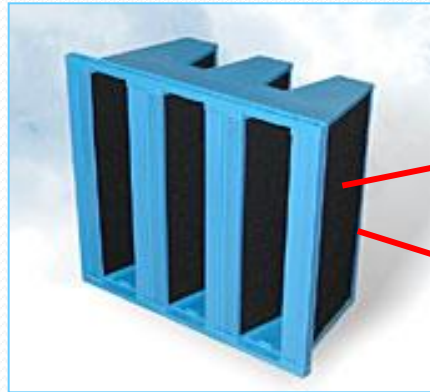
# Gas-Phase Air Filtration Principles (cont.)

Irreversible chemical fixation  
between molecule and impregnation

No Desorption



# Chemical filters



**Chemical filter**

**construction**

**loading**

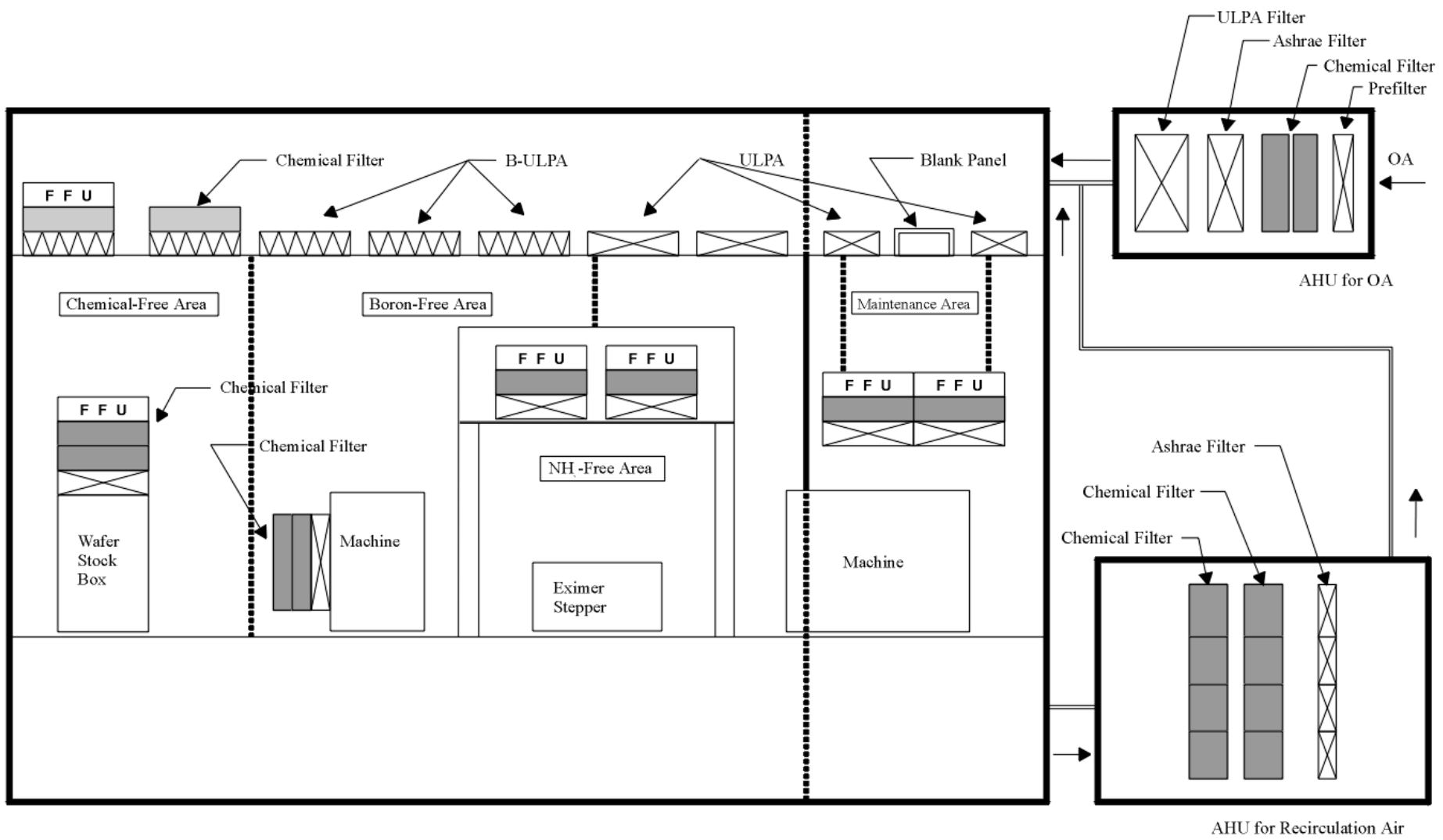
**media**



技術研發



# Filter installation Locations



# Filter Pressure drop & Eff. (Molecular Filter)

